

OMB Control No: xxxx-xxxx
 Expiration Date: xx/xx/xxxx
[Review Draft](#)

Did any of the responses (individual cells) you entered in this tab contain CBI?
 If yes, be sure to shade the CBI-containing cells red and follow the instructions in section C of the survey overview document for submitting CBI.

UK = Unknown. NA = Not Applicable. See instruction document for details on use of these terms.
 "Nominal daily throughput capacity" is defined as the typical operating rate for the emission unit.

Pulp and Paper sector facility data.

	<p>Provide for all entries. This should match NEI Site ID used in Part II of this survey (the NEI update).</p> <p>If no NEI Site ID exists for your facility in Part II, use a temporary ID of "NEW _____" where the blank is your facility's zip code.</p>	Name of legal operator of facility	Complete street address of facility (physical location)					Provide mailing address if different than physical location				Facility contact able to answer technical questions about the con		
Instruction:														
Survey reference:														
Field:	NEI Site ID	Legal operator	Physical address	Physical city	Physical state	Physical zip	Physical county	Mail address	Mail city	Mail state	Mail zip	Mail county	Facility contact name	Facility contact title
Example entry:	99999	Gaint Corporation	1000 Plant Road	Anytown	VA	24553	Amherst	PO Box 123	Fairspring	VA	24554	Amherst	Joe Smith	Environmental Manager

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 "Nominal daily throughput capacity"
Pulp and Paper sector facility data

Instruction: Completed survey	If not the same as legal operator, provide name and address of legal owner of this facility	Dun and Bradstreet Number for the legal owner of this mill (see TRI Form R)	(Optional) Dun and Bradstreet Number for this mill (if the mill has its own Dun and Bradstreet Number) If you operate a non-major source, follow the instructions in the survey overview document for notifying EPA to determine if you should complete this survey. See the 40 CFR part 63 subpart A definition of "major source" in the survey overview document Attachment 1.
Survey reference:			

Field:	Facility contact phone	Facility contact ext	Facility contact fax	Facility contact email	Legal owner address	Legal owner city	Legal owner state	Legal owner zip	Dun Bradstreet owner	Dun Bradstreet mill	HAP size classification
Example entry:	999-999-9999		456 999-999-8888	joe.smith@anymillusa.com	100 Corporate Blvd	Green Bay	WI	54304	9020777	149810921	major

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 "Nominal daily throughput capacity"
Pulp and Paper sector facility data

Instruction: The primary NAICS code represents the line of business that generates the most income for the facility.	Enter the approximate number of employees (worldwide) of the business enterprise that owns this facility, including where applicable, the parent company and all subsidiaries, branches, and unrelated establishments owned by the parent company. Please count full-time, part-time, and temporary employees equally.	Enter the number of facility employees (full-time, part-time, and temporary employees should be counted equally)	The small business size standards for NAICS 322 are based on number of employees of the parent company: 750 employees for NAICS 322110-322130, 322212, and 322215; and 500 employees for all other 322xxx NAICS. See also Attachment 2 of the Part I survey instructions.	Indicate "applies" for each federal NESHAP or NSPS that limits emissions or establishes requirements. Mark "NA" if not applicable (or if the otherwise applicable Federal rule contains no specific requirements) or other standards list the subparts that apply. If in doubt, check your operating permit for Federal air quality requirements.											
Survey reference:	Size of entity			Federal rule coverage											
Field: Example entry:	Primary NAICS 322121-Paper (except Newsprint) Mills	Worldwide employees >1000	Facility employees 500-749	Small business no	<table border="0"> <tr> <td>P&P NESHAP subpart S</td> <td>Combustion Source NESHAP subpart MM</td> <td>Paper/web coating NESHAP subpart JJJ</td> <td>Boiler NESHAP subpart DDDDD (or CISWI emission guidelines/NSPS) that are under development</td> <td>Other NESHAP (list subparts)</td> </tr> <tr> <td>Applies</td> <td>Applies</td> <td>Applies</td> <td>Applies</td> <td>DDDD</td> </tr> </table>	P&P NESHAP subpart S	Combustion Source NESHAP subpart MM	Paper/web coating NESHAP subpart JJJ	Boiler NESHAP subpart DDDDD (or CISWI emission guidelines/NSPS) that are under development	Other NESHAP (list subparts)	Applies	Applies	Applies	Applies	DDDD
P&P NESHAP subpart S	Combustion Source NESHAP subpart MM	Paper/web coating NESHAP subpart JJJ	Boiler NESHAP subpart DDDDD (or CISWI emission guidelines/NSPS) that are under development	Other NESHAP (list subparts)											
Applies	Applies	Applies	Applies	DDDD											

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 Pulp and Paper sector facility data

<p>; from any single piece of equipment at the mill. ents for the equipment types at your mill). For the rule subparts that apply.</p>									Enter the 2009 nominal daily production capacity total for all market pulp products.	Select from menu	
Instruction:				Select yes/no	Select the most relevant response	Select yes/no	Select yes/no	Select from menu. You may write in more than once choice.	Enter number		
Survey reference:				Pulps				Pulp dryers	Market pulp	Bleaching (or brightening) systems	
Field:	Kraft NSPS subpart BB	Boiler NSPS	Other NSPS (list subparts)	Does the mill produce virgin pulp?	Does the mill produce pulp from secondary fiber?	Does the mill purchase virgin pulp?	Does the mill purchase secondary fiber pulp?	Types of market pulp produced by the mill	Total number of pulp dryers used to produce market pulp	2009 nominal daily market pulp production capacity (short tons/day)	Is bleaching or brightening performed at the mill?
Example entry:	Applies	Db	NA	yes	no	no	no	NA	NA	NA	yes-bleaching

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"Nominal daily throughput capacity"
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Instruction:	Enter number of machines	Enter the 2009 total nominal daily production capacity for all paper/paperboard products.	Enter decimal percent for utilization (e.g., 0.7 for 70% of capacity utilized). See survey instructions for an example.	Enter the typical decimal percent for utilization (e.g., 0.7 for 70% of capacity utilized) for the past 5 years. One way to determine the 5-year utilization would be to average the utilization percentages for 2005, 2006, 2007, 2008, and 2009.	Select from menu the general paper grades manufactured by the paper mill in 2009 (noting the product produced in the greatest quantity as product 1, product produced in the 2nd greatest quantity as product 2, etc.)	Use the paper grades most closely related to the paper grades produced at your mill if you do not find an exact match in the menu.	Specify other paper grade(s) if none of the grades in the menu reasonably match the grades produced at your mill		
Survey reference:	Paper or paperboard processes/products		Paper capacity utilization		Paper grades produced				
Field:	Total number of paper machines	2009 nominal daily production capacity total for paper/paperboard (air dried short tons/day)	2009 paper/paperboard capacity utilization percentage	5-year average (2005-2009) paper/paperboard capacity utilization percentage	Paper grade 1	Paper grade 2	Paper grade 3	Paper grade 4	Paper grade 5
Example entry:	1	340000	0.8	0.95	uncoated free sheet	linerboard	other - specialty food-grade		

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Instruction: Optional. Enter any comments you have on the data supplied.

Survey reference:

Field:	Paper grade 6	Paper grade 7	Paper grade 8	Paper grade 9	Paper grade 10	Comments
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Example entry:

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Complete for emission units (as shown in the Emission Unit ID column) with alternate/backup controls used only during certain times. (Primary controls for the collection system were identified in the APCD columns to the left). Specify conditions Specify

Instruction: _____
Survey Reference: _____

Field:	Alternate method of control (specify APCD ID or Emission Unit ID)	Conditions when alternate control is used	Approximate hr/yr when alternate control is used to control emissions from the Emission Unit ID
Example entry:			
	TO	When Boiler EVSS is not operating	330
	TO	When LK1 is not operating	390

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Select yes/no.

[Consider how the emission unit is permitted when specifying if it is subject to NSPS BB. For example, a boiler or thermal oxidizer controlling BB emission units is not necessarily an emission unit subject to BB. If your permit indicates the unit is subject to BB then indicate "yes" in the column below.]

Indicate NSPS BB TRS compliance option used to demonstrate NSPS compliance with primary method of control.

Indicate NSPS subpart BB TRS compliance option used to demonstrate compliance using backup method of control for the emission unit (if a backup method of control is used).

Provide year. If not known, enter approximate year (e.g., "pre-1990")

Select from menu.

[Note: You may enter the compliance option for each emission unit or for the relevant collection system if listed separately. Leave blank if not applicable.]

[Note: Leave blank if no backup control is specified in the columns to the left for this emission unit.]

Instruction:
Survey Reference:
 Subpart BB NSPS applicability

Field:	Is emission unit subject to NSPS BB?	If yes, year became subject to BB (XXXX)	Reason subject to BB	Specify TRS compliance option used to demonstrate NSPS subpart BB compliance (if applicable)	Specify TRS compliance option used for backup method of control (if applicable)
Example entry:	yes	pre-1990	new		
	yes	pre-1990	new		
	no				
	yes	pre-1990	collects emissions from BB emission units	combust gases in lime kiln or recovery furnace subject to subpart BB	5 ppmv @ 10% O2 (combustion control)
	no				
	yes	pre-1990	new		
	no				

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Select yes/no.
 Synthetic area sources should select "no."
 [Consider how the emission unit is permitted when specifying if it is subject to subpart 5. For example, a boiler or TO controlling subpart 5 emission units is not necessarily an emission unit subject to subpart 5. If your permit indicates the unit is subject to subpart 5 then indicate "yes" in the column below.]
 Indicate compliance option met using primary method of control for the emission unit.
 Indicate compliance option met using backup method of control for the emission unit (if a backup method of control is used).
 See pull down menu for potential reasons some vent gas streams may not be covered under subpart 5. Some rule exceptions are listed in the menu, along with a selection for synthetic area sources. You may write in other reasons.
 Complete for each digester source. This could include multiple emission units that are part of one emission source (as noted in the Part 1 survey instructions for "Multiple emission units ducted to a single release point").
 Select from menu. In the menu, "HW/SW swing" refers to digesters that process hardwood (HW) some of the time and softwood (SW) at other times. "HW and SW" refers to digesters that process a mixture of hardwood and softwood. You may also select "Non-wood."
 Enter numeric value
 Enter numeric value
 Enter the types of washers used in series:
 V-vacuum drum
 D-diffusion
 P-pressure
 B-belt
 O-other
 Complete for each pulp washing system. (e.g., washing line).
 Enter number of washers in series
 Pulp washing systems:
 Enter the final washing stage concentration in milligrams per liter. If known, use the average from 2009 or target value.
 If you have vacuum drum washers, enter the final washing stage concentration in milligrams per liter. If known, use the average from 2009 or target value.

Instruction:
Survey Reference:

Field:	Is emission unit subject to NESHAP subpart 5?	Subpart 5 compliance option used (for primary method of control)	Subpart 5 compliance option used (for backup method of control, if applicable)	Provide reason if not controlled to meet subpart 5	Batch or continuous	Digester nominal daily production capacity, ADTP/d	Wood type (HW, SW, HW/SW swing)	Washing system nominal daily production capacity, ADTP/d	Total number of washers	Washer types and sequence	Source of vacuum drum washer final stage shower water	Vacuum drum washer final stage shower water methanol concentration, mg/l
Example entry:	yes				Continuous	480 SW						
	yes				Continuous	520 HW/SW swing						
	yes	Use a boiler, LK, or RF in which the HAP gas stream is introduced with the primary fuel into the flame zone	Reduce total HAP concentration at the outlet of thermal oxidizer to <20 ppmv @ 10% O2 (dry basis)									
	yes	Use a boiler, LK, or RF in which the HAP gas stream is introduced with the primary fuel into the flame zone	Reduce total HAP concentration at the outlet of thermal oxidizer to <20 ppmv @ 10% O2 (dry basis)									
	no											
	no											
	no							1000	3 D.V.V		Striped digester and evaporator condensates	

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ORM Control No: Expiration Date: <small>You may find it helpful to use Excel's</small> UK = Unknown, NA = Not Applica						
Instruction: <small>Knitter, screen, and decker.</small> Enter numeric value		Instruction: <small>Complete for each evaporator system</small> Enter numeric value		Instruction: <small>Complete for oxygen delignification systems.</small> Enter numeric value		
Survey Reference: <small>Knitter, screen, and deckers</small>		Survey Reference: <small>Evaporators</small>		Survey Reference: <small>Oxygen delignification</small>		
Field:	<small>Knitter, screen, or decker nominal daily production capacity, ADTP/d</small>	<small>Type of shower water used in decker</small>	<small>Evaporator nominal daily production capacity, gal/day of weak black liquor</small>	<small>Which pulp washer(s) are the source(s) of weak liquor for the evaporator set?</small>	<small>How many evaporator effects are there?</small>	<small>Methanol concentration in post-O2 delignification washer shower water, mg/l</small>
Example entry:						
			1000 WASHER		6	
	300					1100 WASHER
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Expiration Date: _____										
You may find it helpful to use Excel's _____										
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Hidden columns: Additional supplemental fuel columns (for types 2-6) are hidden. Unhide and complete these columns if relevant.										
<p>Complete for fuel-fired equipment such as boilers, thermal oxidizers, controlling Part 1 emission sources, and direct-fired dryers. Enter the types of supplemental or other fuels fired (excluding SGC or other MCCs).</p> <p>Note that information for recovery furnaces (also known as "recovery boilers" or "black liquor boilers") and lime kilns is to be supplied under Part II of the pulp and paper survey (not Part I).</p> <p>Include secondary and additional fuels used routinely for multi-fuel fired equipment in these columns.</p> <p>Supplemental or other fuels for fuel-fired equipment:</p>										
<p>Enter decimal percent (e.g., 1 = 100% or 0.3 = 30%).</p> <p>Approximations based on the average from 2009 or a target value will suffice.</p>										
<p>Enter the numeric higher heating value (HHV) for non-fossil fuels corresponding to the suggested units in next column.</p> <p>Optional: EPA can assume default HHVs for fossil fuels, or you may opt to enter the HHV for your fossil fuel (e.g., if the fuel is relatively uncommon).</p>										
<p>Specify units corresponding to the HHV. Use _____ for liquid fuels, _____ (dry basis) for solid fuels, and _____ for gaseous fuels.</p>										
<p>Select from menu or write in. You may write in more than one condition.</p>										
<p>Supply startup/shutdown information for equipment (including collection systems or APCDs) that appear in the Emission Unit ID column (except thermal oxidizers). Enter startup/shutdown information for thermal oxidizers in the P1 Controls tab.</p> <p>Enter approximately how long it takes for the emission unit to startup. Use decimals if less than one hour (e.g., 18 minutes = 0.3 hr).</p> <p>Supply information for routine startup and shutdown events such as events associated with planned mill downtime. (Do not provide information for startup/shutdown events associated with control device or emission unit malfunctions).</p> <p>"Startup" means the setting in operation of an affected source or portion of an affected source for any purpose.</p> <p>Emission Unit Startup and Shutdown</p>										
<p>Enter approximately how long it takes for the emission unit to shutdown. Use decimals if less than one hour (e.g., 18 minutes = 0.3 hr).</p> <p>"Shutdown" means the cessation of operation of an affected source or portion of an affected source for any purpose.</p>										
<p>Write in response specifying when startup ends and normal operation begins (e.g., Startup ends when the auxiliary burners switch off and material throughput begins to flow.)</p> <p>Select from menu or write in</p>										
<p>Select from menu or write in</p>										
Field:	Supplemental fuel type 1	Approximate percent of annual heat input capacity (HHV/yr) supplied by supplemental fuel 1 (fossil)	Optional: Supplemental fuel type 1 HHV (if non-fossil)	Optional: Supplemental fuel type 1 HHV units	Conditions when supplemental fuel type 1 used	Approximate duration of emission unit startup (hours)	Measures employed to reduce air emissions during emission unit startup (if any)	What marks the end of emission unit startup and beginning of normal operating conditions?	Approximate duration of emission unit shutdown (hours)	Measures employed to reduce air emissions during shutdown (if any)
Example entry:						0.5	backupalternate control	When full pulp flow from the digester is obtained	1	continue routing emissions to LVHC 1 collection system and primary or backup control system
						0.5	backupalternate control	When full pulp flow from the digester is obtained	1	continue routing emissions to LVHC 1 collection system and primary or backup control system
						2	backupalternate control	stripper steam application rate reaches target; and begin flow of process condensates from tank	1	stop routing process condensates to stripper before beginning shutdown
						0.1	backupalternate control	flow through bypass ceases	0.2	NA - applicable emission and parameter limits not expected to be exceeded during shutdown
	natural gas	0.05			startup, backup	12	Operate WESP during boiler startup	Steam pressure of 100 psig or greater achieved	12	emission unit and control device operates during emission unit startup (but not necessarily in compliance with all NSPS/NESHAP parameter limits)
						18	backupalternate control	Stripper liquor flow of 600 gpm at evaporator exit (55% solids)	16	continue routing emissions to LVHC 1 collection system and primary or backup control system
						12	emission unit and control device operates in compliance with NSPS and NESHAP parameter limits during emission unit startup	Combustion temperature is reached	14	Temperature drops below 200F

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ORM Control No: Expiration Date: <small>You may find it helpful to use Excel's</small> UK = Unknown, NA = Not Applica		
	Write in response specifying when shutdown begins and normal operation ends (e.g. Shutdown begins when material throughput ceases to flow.)	OPTIONAL QUESTION. Input on appropriate standards that would be reasonable for your pulp and paper source category emission units is requested. Supply recommendations for the specific equipment (including collection systems or APCDs) appearing in the Emission Unit ID column. Optional. Enter any comments you have on the data supplied.
Instruction:		
Survey Reference:		
	Optional: Do you wish to recommend a standard that would apply during startup or shutdown of this emission unit? If so, please describe the event to which the standard would apply; the recommended standard (this could be an emission limitation, work practice, or operational standard) that would apply during the period; the basis for the recommended standard; why and how the standard would minimize emissions during the event; and how would compliance be determined and/or monitored. Supply as a separate attachment to your survey response if necessary.	
Field:	What marks the end of normal operating conditions and beginning of emission unit shutdown?	Comments
Example entry:	Stop transfer of wood chips from the feed silo	Rule could require continued routing of emissions to VPM-1 collection system and primary and/or backup control system during digester startup and shutdown.
	Stop transfer of wood chips from the feed silo	Rule could require continued routing of emissions to VPM-1 collection system and primary and/or backup control system during digester startup and shutdown.
	shut off steam supply to the stripper	Rule could require continued routing of SOG to existing primary and/or backup control system during stripper startup and shutdown.
	flow through bypass begins	
	Stop charging hog fuel into boiler	
	Steam flow to first effect reduced by 50%	Rule could require continued routing of emissions to VPM-1 collection system and primary and/or backup control system during evaporator startup and shutdown.
	Cease flow of liquor through injection nozzles	

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OMB Control No: XXXX-XXXX
 Expiration Date: xx/xx/xxxx

Review Draft

UK = Unknown. NA = Not Applicable. See instruction document for details on use of these terms.

Pulp and Paper sector permit data You do not need to complete this tab for boilers.

<p>Instruction: Survey reference:</p>	<p>Provide for all entries. This should match NEI Site ID used in Part II.</p>	<p>Provide for all entries. Use the Emission Unit ID in the <i>PI Equip detail</i> tab if the individual emission unit was listed there. If emission units are aggregated by a collection system then you may need to use the Collection system ID from the <i>PI Equip detail</i> tab.</p>	<p>OPTIONAL column useful for cross-checking permit data and when comparing permit to NEI.</p>	<p>Select from menu or write in</p>	<p>OPTIONAL. Complete this column to avoid restating Federal permit limits in the columns to the right.</p>	<p>Enter numeric value of permit limit coinciding with the pollutant selected.</p> <p>You <u>do not</u> have to provide every limit for pollutants with multiple limits in different units of measure.</p> <p>See the survey instruction document for permit limit units of interest.</p>
<p>Field:</p>	<p>NEI Site ID</p>	<p>Emission Unit ID or Collection System ID</p>	<p>Identifier used in permit (e.g., emission unit ID, stack ID, etc) - optional</p>	<p>Pollutant</p>	<p>If the permit limit is identical to the Federal NESHAP or NSPS limit, you may enter the NESHAP/NSPS subpart here rather than restating the Federal limit in the columns to the right</p>	<p>Numeric permit limit 1</p>
<p>Example entry:</p>	<p>99999</p>	<p>EU30</p>	<p>EU30_1</p>	<p>PM - filterable</p>		<p>0.02</p>
	<p>99999</p>	<p>EU30</p>	<p>EU30_1</p>	<p>Opacity</p>		<p>5</p>

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Field:	NEI Site ID	Emission Unit ID or Collection System ID	Identifier used in permit (e.g., emission unit ID, stack ID, etc) - optional	Pollutant	If the permit limit is identical to the Federal NESHAP or NSPS limit, you may enter the NESHAP/NSPS subpart here rather than restating the Federal limit in the columns to the right	Numeric permit limit 1
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Field:	NEI Site ID	Emission Unit ID or Collection System ID	Identifier used in permit (e.g., emission unit ID, stack ID, etc) - optional	Pollutant	If the permit limit is identical to the Federal NESHAP or NSPS limit, you may enter the NESHAP/NSPS subpart here rather than restating the Federal limit in the columns to the right	Numeric permit limit 1
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Field:	NEI Site ID	Emission Unit ID or Collection System ID	Identifier used in permit (e.g., emission unit ID, stack ID, etc) - optional	Pollutant	If the permit limit is identical to the Federal NESHAP or NSPS limit, you may enter the NESHAP/NSPS subpart here rather than restating the Federal limit in the columns to the right	Numeric permit limit 1
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Field:	NEI Site ID	Emission Unit ID or Collection System ID	Identifier used in permit (e.g., emission unit ID, stack ID, etc) - optional	Pollutant	If the permit limit is identical to the Federal NESHAP or NSPS limit, you may enter the NESHAP/NSPS subpart here rather than restating the Federal limit in the columns to the right Numeric permit limit 1
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Field:	NEI Site ID	Emission Unit ID or Collection System ID	Identifier used in permit (e.g., emission unit ID, stack ID, etc) - optional	Pollutant	If the permit limit is identical to the Federal NESHAP or NSPS limit, you may enter the NESHAP/NSPS subpart here rather than restating the Federal limit in the columns to the right	Numeric permit limit 1
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Field:	NEI Site ID	Emission Unit ID or Collection System ID	Identifier used in permit (e.g., emission unit ID, stack ID, etc) - optional	Pollutant	If the permit limit is identical to the Federal NESHAP or NSPS limit, you may enter the NESHAP/NSPS subpart here rather than restating the Federal limit in the columns to the right	Numeric permit limit 1
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Field:	NEI Site ID	Emission Unit ID or Collection System ID	Identifier used in permit (e.g., emission unit ID, stack ID, etc) - optional	Pollutant	If the permit limit is identical to the Federal NESHAP or NSPS limit, you may enter the NESHAP/NSPS subpart here rather than restating the Federal limit in the columns to the right	Numeric permit limit 1
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OMB Control No:
 Expiration Date:
 Review Draft

UK = Unknown. NA = I

Pulp and Paper sector

<p>Instruction: Survey reference:</p>	<p>Supply averaging time for permit limit if an averaging time is specified in the permit. Averaging times are commonly specified for pollutants measured with continuous monitors (e.g., 3-hour block average, daily average, etc).</p> <p>Leave blank if no averaging time is specified in your permit.</p> <p>Enter units for permit limit</p>	<p>Enter numeric value of permit limit coinciding with the pollutant selected.</p> <p>You <u>do not</u> have to provide every limit for pollutants with multiple limits in different units of measure.</p> <p>See the survey instruction document for permit limit units of interest.</p> <p>Enter units for permit limit</p>	<p>Supply averaging time for permit limit if an averaging time is specified in the permit. Averaging times are commonly specified for pollutants measured with continuous monitors (e.g., 3-hour block average, daily average, etc).</p> <p>Leave blank if no averaging time is specified in your permit.</p> <p>Enter units for permit limit</p>	<p>Enter numeric value of permit limit coinciding with the pollutant selected.</p> <p>You <u>do not</u> have to provide every limit for pollutants with multiple limits in different units of measure.</p> <p>See the survey instruction document for permit limit units of interest.</p> <p>Enter units for permit limit</p>
<p>Field:</p>	<p>Units for permit limit 1 (including any applicable %O2 or %CO2 correction factors)</p> <p>Averaging time for permit limit 1 (if applicable)</p>	<p>Numeric permit limit 2</p> <p>Units for permit limit 2 (including any applicable %O2 or %CO2 correction factors)</p> <p>Averaging time for permit limit 2 (if applicable)</p>	<p>Numeric permit limit 3</p> <p>Units for permit limit 3 (including any applicable %O2 or %CO2 correction factors)</p>	
<p>Example entry:</p>	<p>gr/dscf @ 8% O2</p> <p>% opacity</p> <p>6-min avg</p>	<p>20 % opacity</p>	<p>Do not exceed 20% for more than three 6-min averages in a 3-hour period determined by Method 9</p>	

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UK = Unknown. NA = I

Pulp and Paper sector

<p>Instruction: Survey reference:</p>	<p>Supply averaging time for permit limit if an averaging time is specified in the permit. Averaging times are commonly specified for pollutants measured with continuous monitors (e.g., 3-hour block average, daily average, etc). Leave blank if no averaging time is specified in your permit.</p>	<p>Enter numeric value of permit limit coinciding with the pollutant selected. You <u>do not</u> have to provide every limit for pollutants with multiple limits in different units of measure. See the survey instruction document for permit limit units of interest.</p>	<p>Enter units for permit limit</p>	<p>Supply averaging time for permit limit if an averaging time is specified in the permit. Averaging times are commonly specified for pollutants measured with continuous monitors (e.g., 3-hour block average, daily average, etc). Leave blank if no averaging time is specified in your permit.</p>	<p>Enter numeric value of permit limit coinciding with the pollutant selected. You <u>do not</u> have to provide every limit for pollutants with multiple limits in different units of measure. See the survey instruction document for permit limit units of interest.</p>	<p>Enter units for permit limit</p>	<p>Supply averaging time for permit limit if an averaging time is specified in the permit. Averaging times are commonly specified for pollutants measured with continuous monitors (e.g., 3-hour block average, daily average, etc). Leave blank if no averaging time is specified in your permit.</p>
<p>Field:</p>	<p>Averaging time for permit limit 3 (if applicable)</p>	<p>Numeric permit limit 4</p>	<p>Units for permit limit 4 (including any applicable %O2 or %CO2 correction factors)</p>	<p>Averaging time for permit limit 4 (if applicable)</p>	<p>Numeric permit limit 5</p>	<p>Units for permit limit 5 (including any applicable %O2 or %CO2 correction factors)</p>	<p>Averaging time for permit limit 5 (if applicable)</p>
<p>Example entry:</p>							

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OMB Control No:
Expiration Date:

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Pulp and Paper sector

Instruction:	Optional. Enter any comments you have on the data supplied.
Survey reference:	
Field:	Comments
Example entry:	

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Complete this table for add-on air pollution controls. Questions regarding combustion controls and process changes are included elsewhere in other survey tabs.
UK = Unknown. NA = Not Applicable. See instruction document for details on use of these terms.
 You do not need to complete this tab for boiler air pollution control devices.

Instruction:	Provide for all entries. This should match NEI Site ID used in Part II.		Enter Emission Unit ID or Collection system ID matching the Equip detail tab.	Note: If control device serves as a backup control.	Select from menu or write in	Enter the manufacturer of the APCD, if known. Enter "UK" for unknown. Enter "shop-built" for equipment designed by the mill.	Enter the year installed, if known. Enter "UK" if unknown; or "pre-1990" if more than 20 years old and the install date is unknown. If the APCD was substantially upgraded, enter the year of the upgrade as "XXXX."	Enter the typical pressure drop across the control device in inches of water P-drop	Control efficiency	"Actual" control efficiency is a measured value obtained through inlet/outlet emissions testing. Leave blank if not known or not applicable.	Include control efficiency for specific HAP that you identify. This may be HAPs used as surrogates in a rule (e.g., methanol, chlorine) or other HAP.	You may attach a separate listing of HAPs and control efficiencies if this information is available for a number of compounds.	Complete for thermal oxidizers or incinerators used to control Part I emission sources. Select from list	Enter number of canisters (media beds) for a regenerative thermal oxidizer (RTO)	Enter target firebox combustion/operating temperature (F)	Enter time stack gases are exposed to the target temperature (actual or design value)	Select yes/no	Select from list or write in	
Field:	NEI Site ID	APCD ID	Emission Unit ID(s) or Collection system ID(s)	Type of control device	APCD manufacturer (if known)	Year installed (XXXX)	Pressure drop, in. H2O	Actual PM control efficiency (if known), %	Actual TRS control efficiency (if known), %	Actual HCl control efficiency (if known), %	Actual SO2 control efficiency (if known), %	Actual HAP control efficiency (if known), %	Specify HAP	Incinerator type	If RTO, number of canisters	Target firebox temperature (F)	Residence time at operating temperature (sec)	Heat recovery	What is the recovered heat from the incinerator exhaust used for?
Example entry:		99999 ANYCONTROL	ANYUNIT	ANYTYPE	UK	pre-1990	4	98				90	Methanol						
		99999 SCRB2	LK1_LVHCL	Scrubber	Ducon	1985	6	95	92		82	50	Formaldehyde, Methanol						
		99999 TO	STRIPPER (backup); LVHCL (backup)	Thermal oxidizer/incinerator	Coen	1999	2							Single-stage combustion chamber	NA	1300	1.8	no	NA

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Complete this table for add-on air pollution control equipment.
UK = Unknown. NA = Not Applicable.
You do not need to complete this table if you have no add-on air pollution control equipment.

Instruction:	Complete the sorbent injection questions for sorbents injected into the gas stream prior to collection by a fabric filter or other control device for which information is being provided. For example, complete the sorbent injection questions for a dry injection fabric filter system in the same row where you enter information for the fabric filter.	Select from list or write in	Enter pounds per hour (lb/hr) of sorbent injected into the exhaust gas stream. Use the average from 2009 or a target value.	Indicate the filter material and note if coatings are added to the filter material (e.g., polyester with PTFE coating). If no coating is indicated (e.g., polyester), the filter material is uncoated.	Select from list	Enter typical bag life (or expected bag life), in months	Enter number of fabric filter compartments. Enter "1" if the baghouse is not separated by different compartments.	Enter the design air-to-cloth ratio (gas flow divided by the filter bag material area)	Complete the ESP questions for dry ESPs and WESPs	Enter number of fields used during normal operation. This may be the same as the total number of fields unless some fields are offline (e.g., for cleaning).	Enter the design specific collection area (area of the plates divided by gas flow rate).	Describe any ESP upgrades made within the last 10 years, such as addition of fields or other upgrades to increase ESP efficiency. If no upgrades, leave blank.	Complete these additional ESP questions for WESPs.	If a quench is used prior to the ESP, complete the scrubber questions for the quench.	Include water flow through the WESP. Use the average from 2009 or a target value.	Complete for all types of wet scrubbers (venturi, tray, plate, injection, quench, etc.)	Enter the numeric value for the scrubber design liquid-to-gas ratio (L/G) in gallons of liquid per 1000 acfm of gas. Use the average from 2009 or a target value.	Enter numeric value for the target pH. Use the average from 2009 or a target value.	Enter typical gallons per minute of scrubbing fluid (e.g., water) make-up added to the system. Use the average from 2009 or a target value.	Select yes/no for scrubbers that control chemical recovery furnaces or Semichemical liquor combustion units. Leave blank for other scrubbers.	Complete the scrubber questions and complete the additional questions below related to the packing material
Survey reference:	Sorbent injection			Fabric filters					ESPs				WESPs			Scrubber					Packed bed scrubbers/absorbers
Field:	Sorbent type	List pollutants the sorbent injection was installed to control	Sorbent injection rate, lb/hr	Filter material and added coatings	Bag cleaning method	Typical bag life (months)	Number of compartments	Air-to-cloth ratio (acfm/ft ²)	Total number of fields	Number of fields used during normal operation	Specific collection area, ft ² /1,000 acfm	Have fields/chambers been added to expand the ESP within the last 10 years?	Is WESP preceded by a quench chamber	WESP water flow, gpm	Type of alkali added, if any	Liquid-to-gas ratio (gal/1000 acfm)	Inlet pH of scrubbing liquid	Scrubbing fluid make-up rate, gpm	For recovery furnaces/combustion units: Does scrubber also serve as a direct contact evaporator?	Type of packing material	Packing material depth, ft
Example entry:	activated carbon	Hg	100	Polyester	Shake	15	1	7	8	4	466	No	No	275			8	130	No	plastic packing	3
															Caustic	6	10	60			

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Complete this table for add-on air pc
 UK = Unknown. NA = Not Applicable
 You do not need to complete this table

Instruction:		Select yes/no		Do not include spent pulping liquor used in recovery furnace wet bottom ESPs here (as information for wet bottom ESPs is requested in the PI Equip detail tab).		Do not include baghouses or cyclones used solely for wood/material handling operations.		Do not include baghouses or cyclones used solely for wood/material handling operations.		Do not include baghouses or cyclones used solely for wood/material handling operations.		Do not include baghouses or cyclones used solely for wood/material handling operations.		Do not include baghouses or cyclones used solely for wood/material handling operations.	
Survey reference:		Water source and usage		Water source and usage		Water source and usage		Water source and usage		Water source and usage		Water source and usage		Water source and usage	
Field:	Scrubber/absorber cross-sectional area, ft²	Water source	Is water recirculated?	Water recirculation rate, gpm	Wastewater (blowdown) %	Wastewater (blowdown) reuse or disposal method	Type of material collected	End use/method of disposal for solid material collected	Solid material disposed (if known), cu yd/yr	Identify any other solid waste associated with the APCD	Frequency of material replacement/disposal	End use/method of disposal for solid material collected	Amount of material to be disposed (if known), cu yd	List continuous parameter monitoring systems used for this control device (e.g., pressure drop, liquid flow)	Please list below any additional operating parameters that are either monitored or that are important for proper operation of the APCD, and include average values and units.
Example entry:	19.6	treated wastewater	Yes	200	0.1	Treated in onsite wastewater treatment plant	carbon sorbent laden with PM	landfill onsite	410	degraded packing material	5 yr	landfill offsite	0.5	liquid flow, voltage	carbon injection rate (100 lb/hr)
		surface water and water from recirculation pond	Yes	350	0.35	Treated in onsite wastewater treatment plant								pressure drop, liquid flow rate	
														combustion chamber temperature	

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Complete this table for add-on air po
 UK = Unknown. NA = Not Applic
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OPTIONAL: Supply approximate capital costs of the parameter monitoring system equipment installed within the past 10 years for this control device. Include in the equipment costs the analyzer and data acquisition system (DAS), if known.

OPTIONAL: Enter year for parameter monitoring system costs

Supply startup/shutdown information for the equipment that appears in the APCD ID column.

Enter approximately how long it takes for the control device to startup. Use decimals if less than one hour (e.g., 18 minutes = 0.3 hr).

Supply information for routine startup and shutdown events such as events associated with planned mill downtime. (Do not provide information for startup/shutdown events associated with control device or emission unit malfunctions).

"Startup" means the setting in operation of an affected source or portion of an affected source for any purpose.

Control Device Startup and Shutdown

List any control device parameter limits that cannot be met during control device startup. Certain parameters may be "instant on" while others are more transient in nature. Examples could include control device temperature that must heat up to a set point, or pressure drop that cannot be achieved due to low exhaust gas flow from the emission unit.

The EPA is particularly interested in emission limits or parameter limits originating from the pulp and paper NSPS or NESHAP that cannot be met during control device startup or shutdown.

Select from menu if the applicable emission and parameter limits are expected to be met during startup.

Select from menu, expand on menu response, and/or write in.

For example, is a certain gas flow rate from the emission unit required before the control device operating parameter limits can be met? Is a certain heating value from the emission unit exhaust gas required to achieve control device temperature?

Write in response (if any).

Write in response specifying when control device startup ends and normal operation begins (e.g., Startup ends when oxidizer temperature set point of 1200F is reached.)

Enter approximately how long it takes for the control device to shutdown. Use decimals if less than one hour (e.g., 18 minutes = 0.3 hr).

"Shutdown" means the cessation of operation of an affected source or portion of an affected source for any purpose.

Select from menu, expand on menu response, and/or write in.

For example, is a certain gas flow rate from the emission unit required for the control device operating parameter limits to be met? Is a certain heating value from the emission unit exhaust gas required to achieve control device temperature?

Survey reference:

Field:	Capital costs of parameter monitoring system, \$	Base year for parameter monitoring system capital cost (e.g., 2005)	Approximate duration of control device startup (hours)	Explain how control device startup is integrated with (dependent upon) emission unit startup/operation	List any control device continuous emissions monitoring or operating parameter limits that cannot be met during control device startup	Measures employed to reduce air emissions during control device startup (if any)	What marks the end of control device startup and beginning of normal operating conditions?	Approximate duration of control device shutdown (hours)	Explain how control device shutdown is integrated with (dependent upon) emission unit shutdown
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Example entry:			0.4	Need airflow from emission unit of at least 10,000 acfm in order for injected carbon to properly mix and become entrained in gas stream	carbon injection rate	Ensure water is recirculated through control device throughout startup	route emission unit exhaust damper to control device and switch on carbon injection once process exhaust gas reaches 10,000 acfm	0.4	Need airflow from emission unit of at least 10,000 acfm in order for injected carbon to properly mix and become entrained in gas stream
	34500	2007	3	Control device cannot function as designed unless an air flow rate of 29,000 acfm from the emission unit is achieved.	pressure drop	meet liquid flow parameter limit	Startup ends when the pressure drop parameter limit range is achieved	0.5	Control device cannot function as designed unless an air flow rate of 29,000 acfm from the emission unit is achieved.
	22000	1999	4		temperature set point	bring TO temperature to 1400F before routing NCG or SOG to the TO	Combustion temperature reaches 1400F	4	Control device continues to operate and meets required operating limits while emission unit is shut down or re-routed.

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UK = Unknown. NA = Not Applic
 You do not need to complete this ta

List any control device parameter limits that cannot be met during control device shutdown. Certain parameters may be "instant off" while others are more transient in nature. Examples could include control device temperature that decreases from the set point as shutdown progresses, or pressure drop that cannot be achieved due to low exhaust gas flow from the emission unit.

The EPA is particularly interested in emission limits or parameter limits originating from the pulp and paper NSPS or NESHAP that cannot be met during control device startup or shutdown.

Select from menu if the applicable emission and parameter limits are expected to be met during shutdown.

Write in response specifying when shutdown begins and normal operation ends (e.g., Shutdown begins when the burners are shut off.)

OPTIONAL QUESTION. Input on appropriate standards that would be reasonable for your pulp and paper source category control system is requested. Supply recommendations for the specific APCD appearing in the APCD ID column.

Optional. Enter any comments you have on the data supplied.

Field:	List any control device continuous emissions monitoring or operating parameter limits that cannot be met during control device startup	Measures employed to reduce air emissions during control device shutdown (if any)	What marks the end of normal operating conditions and beginning of control device shutdown?	Optional: Do you wish to recommend a standard that would apply during startup or shutdown of this control device? If so, please describe the event to which the standard would apply; the recommended standard (this could be an emission limitation, work practice, or operational standard) that would apply during the period; the basis for the recommended standard; why and how the standard would minimize emissions during the event; and how would compliance be determined and/or monitored. Supply as a separate attachment to your survey response if necessary.	Comments
Example entry:	carbon injection rate	Continue injection of carbon until process gas flow drops to 10,000 acfm; continue water recirculation unit emission unit switched off	When process gas flow drops to 10,000 acfm and carbon injection is shut off	Require compliance with liquid flow parameter limit during startup and shutdown (but not carbon injection rate limit)	
		Wait until LK is cooled to 200F before switching off liquid flow.	Shut off liquid flow	Meet liquid flow parameter limits during startup and shutdown (but not the pressure drop parameter limit because it can only be achieved during normal operation)	
	temperature set point	Route NCG and/or SOG back to primary control	NCG/SOG re-routed to primary control device	Cease firing NCG or SOG during TO shutdown (route NCG and SOG to primary control device)	

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OMB Control No: xxxx-xxxx
 Expiration Date: xx/xx/xxxx

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Did any of the responses (individual cells) you entered in this tab contain CBI?
 If yes, be sure to shade the CBI-containing cells red and follow the instructions in section C of the survey overview document for submitting CBI.

Use this table for pulp produced onsite. Do not include pulp purchases in this table.
 Mills can have one or more rows in this table depending on the number of pulping processes/lines at the mill.
 Complete the columns that are applicable for each pulp type, leaving the inapplicable columns blank.
UK = Unknown. NA = Not Applicable. See instruction document for details on use of these terms.
 Provide data for the 2009 operating year.

Field:	NEI Site ID	Pulping processes	Operating hr/yr	Unbleached pulp nominal daily production capacity ADTP/d in 2009	Unbleached pulp nominal capacity utilization percentage in 2009	5-year average (2005-2009) unbleached pulp capacity utilization percentage	Chips produced onsite	Chips produced offsite	Sawmill residues	Virgin SW decimal %	Virgin HW decimal%	Approximate percentage of virgin wood pulp that is bleached (or brightened) onsite
Example entry:	99999	kraft	8500	950	0.8	0.95	yes	yes	no	0.2	0.8	NA

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Use this table for pulp produced onsite
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Instruction:		Survey reference:					How does the mill use the pulp it produces from secondary fiber?			Determine the approximate decimal percentage requested based on annual unbleached pulp capacity (ADTP/yr).		This column represents the amount of unbleached pulp that is sold (or transferred to another mill within the same company) as unbleached market pulp. Decimal percent.	This column represents the amount of unbleached pulp that is used onsite to manufacture unbleached paper/paperboard. Decimal percent.		
This column represents the amount of unbleached pulp that is sold (or transferred to another mill within the same company) as unbleached market pulp. Decimal percent.		This column represents the amount of unbleached pulp that is used onsite to manufacture unbleached paper/paperboard. Decimal percent.		Select yes/no			Specify the recycled material used for secondary fiber pulping.			Provide approximate decimal percentages of secondary fiber capacity (ADTP/yr supplied to the left).			This column represents the amount of unbleached pulp that is sold (or transferred to another mill within the same company) as unbleached market pulp. Decimal percent.		This column represents the amount of unbleached pulp that is used onsite to manufacture unbleached paper/paperboard. Decimal percent.
Field:		Approximate percentage of virgin wood pulp sold as unbleached market pulp	Approximate percentage of virgin wood pulp used onsite to manufacture unbleached paper/paperboard?	Check (=1)	For TMP or pressurized groundwood systems, is a heat recovery system used?	Mixed paper decimal%	High grade deinked decimal%	ONP decimal%	OCC decimal%	Pulp substitute decimal%	Approximate percentage of secondary fiber pulp that is bleached (or brightened) onsite	Approximate percentage of secondary fiber pulp sold as unbleached market pulp	Approximate percentage of secondary fiber pulp used onsite to manufacture unbleached paper/paperboard?		
Example entry:		0.25	0.75	1											
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Use this table for pulp produced onsite
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Field:	Check (=1)	Non-wood material	Approximate percentage of nonwood pulp that is bleached (or brightened) onsite	Approximate percentage of nonwood pulp sold as unbleached market pulp	Approximate percentage of nonwood pulp used onsite to manufacture unbleached paper/paperboard?	Check (=1)	Comments
Instruction:		Select from list	Determine the approximate decimal percentage requested based on annual unbleached pulp capacity (ADTP/yr). This column represents the amount of unbleached pulp that typically goes to an onsite bleaching/brightening line.	This column represents the amount of unbleached pulp that is sold (or transferred to another mill within the same company) as unbleached market pulp.	This column represents the amount of unbleached pulp that is used onsite to manufacture unbleached paper/paperboard.		Optional. Enter any comments you have on the data supplied.
Survey reference:		Non-wood pulping material.					
Example entry:	0					0	
1	0					0	
2	0					0	
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Did any of the responses (individual cells) you entered in this tab contain CBI?
 If yes, be sure to shade the CBI-containing cells red and follow the instructions in section C of the survey overview document for submitting CBI.

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UK = Unknown. NA = Not Applicable. See instruction document for details on use of these terms.
 Each pulp mill producing turpentine and/or tall oil should have one row in this table.

Instruction:	Provide for all entries. This should match NEI Site ID used in Part II.	Enter numeric value based on nominal production capacity	Enter numeric value based on nominal production capacity	Insert Emission Unit IDs separated by commas	Enter numeric value based on nominal production capacity	
Survey reference:		Turpentine			Tall oil	
Field:	NEI Site ID	Turpentine production, hr/yr	Turpentine production, gal/yr	Digesters supplying turpentine production (insert Emission Unit IDs)	Tall oil production, ton tall oil/yr	Evaporators supplying tall oil production (insert Emission Unit IDs)
Example entry:	99999	8500	700	DIG-1, DIG-2	220000	EVAP-1, EVAP-2

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UK = Unknown. NA = Not Applicable. §
Each pulp mill producing turpentine and/or

Instruction: Select from menu. Enter numeric value (if batch) Enter numeric value (if batch) Enter numeric value based on nominal production capacity (if continuous) Enter numeric value (if continuous) Optional. Enter any comments you have on the data supplied.
Survey reference:

Field:	Is tall oil acidulation reactor batch or continuous?	Batch reactor cycle time (hr)	Typical batch reactor cycles per day	Continuous or batch tall oil reactor operation, day/yr	Continuous tall oil reactor nominal production capacity, tons tall oil per hour	Comments
Example entry:	continuous			365	25	

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Field:	NPL Site ID	Kraft condensate stream	Emission Unit ID# (or Collection System ID# for HVLC or LVHC systems)	Is condensate stream collected and treated according to subpart 5?	Indicate volume reduction option being used, or other reason why condensate stream is not collected and controlled	For condensates treated by recycling to equipment meeting the Kraft pulping recycle water standards, specify the equipment. Emission Unit ID receives recycled condensates.	For condensates treated by steam stripping, specify the control option used	Date of compliance demonstration(s)	Compliance test results (include units)	For condensates treated by biological treatment, specify the control option used	Date of compliance demonstration(s)	Compliance test results (include units)	Specify condensate treatment method (if other than steam stripping or biological treatment)	Specify the control option used	Date of compliance demonstration(s)	Compliance test results (include units)	Please describe if multiple treatment methods used for this condensate	Comments
<div data-bbox="2252 313 2360 394" style="border: 1px solid black; padding: 2px; width: fit-content; margin-left: auto; margin-right: auto;"> <p>PLM condensate recycling process condensate stream containing a combined total of at least 95 percent of the total HAP from each different stream, separate recovery stream, and separate control according to 40.446(c)(2). PLM collects waste-pulping process condensate stream containing a combined total of at least 75.0 percent.</p> </div>																		

OMB Control No: XXXX-XXXX
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Did any of the responses (individual cells) you entered in this tab contain CBI? If yes, be sure to shade the CBI-containing cells red and follow the instructions in section C of the survey overview document for submitting CBI.

Complete this spreadsheet tab once for each set of CCA compliance calculations used by a mill. As an alternative to completing this tab, you may submit documentation of your CCA calculations used for purposes of showing compliance. You will have 1 row of data in the left-hand table of this tab (emission balance), and multiple rows in the right-hand table in this tab (CCA equipment list). This tab does not apply for synthetic area sources.

Notes:
 Sources eligible for inclusion in the CCA as credit generators include (but are not limited to): pulping systems, bleaching systems, causticizing systems, papermaking systems, and wastewater treatment systems. Debit generating sources can include equipment from the kraft mill HVLC system, including: pulp washing systems, knoter systems, screen systems, O2 delignification systems, and weak liquor storage tanks. Refer to the system definitions in subpart 5 at §63.441 and 63.447(a). If equipment other than that listed above is included in your CCA calculations, please include that equipment in the tab. EPA is not requesting detailed calculations used to show compliance with the CCA at this time. However, EPA reserves the right to request additional detail if needed as a follow-up to this survey.
UK = Unknown. NA = Not Applicable. See instruction document for details on use of these terms.

Emissions Balance Your response will consist of one row on this left side of the orange line.

Instruction: Provide for all entries. This should match NEI Site ID used in Part II. Baseline emissions are measured after compliance has been achieved with the kraft pulping process condensate standards, and the revised effluent limitations guidelines and standards in 40 CFR 430 subpart B. The baseline HAP emissions are determined according to §63.447(d). HAP emission reductions from baseline are required to be determined in §63.447(e).

Survey reference:

Field:	NEI Site ID	Baseline emissions (kg total HAP/Mg ODP)	Emission reductions expected through compliance with the CCA (kg total HAP/Mg ODP)	Year compliance last demonstrated using CCA	How many times has the mill changed the CCA compliance strategy (e.g., changed debit or credit emission points) since first demonstrating compliance with the CCA? Please indicate the year(s) of the change(s).
Example entry:	99999	0.68	0.34	2007	once - 2007

CCA Equipment List Your response will consist of multiple rows on this right side of the orange line.

Instruction: Your response will be multiple rows on this side of the orange line. Complete for each emissions unit involved in a CCA calculation. List each emission unit on a separate row and indicate whether it generates debits or credits in the CCA calculation. Select from menu. List control technology for credit-generating emission units. If applicable, list technology applied for under-controlled debit-generating units as well. List parameters. Optional. Enter any comments you have on the data supplied.

Survey reference:

Field:	NEI Site ID	Emission Unit ID	CCA debit or credit generating emission point?	Clean condensate alternative technology applied	Parameters monitored for clean condensate alternative technology	Comments
Example entry:		99999 BSW1	debit (uncontrolled)	NA-debit source		
		99999 PM2	credit	other - maintain paper machine white water methanol concentration below 20 mg/l by draining a portion of the methanol-concentrated liquid from the pulp stock and replacing it with cleaner water	paper machine throughput; and methanol concentration (mg/l) in the stock blend tanks (SST3), machine chest (PM2MC), and save-all (SVT)	

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Did any of the responses (individual cells) you entered in this tab contain CBI?
 If yes, be sure to shade the CBI-containing cells red and follow the instructions in section C of the survey overview document for submitting CBI.

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Include one row for each bleaching or brightening line located at your mill. Some mills will have only one row, while other mills will have a few rows.
 For example, a mill that produces bleached chemical pulp, bleached secondary fiber pulp, and brightened mechanical pulp could include three rows (one for each type of pulp that is bleached/brightened using separate bleaching/brightening processes).
UK = Unknown. NA = Not Applicable. See instruction document for details on use of these terms.
 Note: The terms "bleaching" and "brightening" should be viewed as interchangeable in this tab (e.g., "Bleaching" can also be read as "Brightening").

Instruction:	Provide for all entries. This should match NEI Site ID used in Part II.	This section (to the left of the orange line) is to be completed by all mills that perform any type of bleaching or brightening.	Select yes/no	Select yes/no	Select from menu. Please explain if the bleaching process cannot be characterized as ECF, PCF, or TCF.	Use the following bleaching sequence notation: C-Chlorine (Cl2) D-Chlorine dioxide (ClO2) E-Alkaline extraction (NaOH etc) P-Hydrogen Peroxide (H2O2) O-Oxygen (O2) H-Hypochlorite (NaClO) Z-Ozone (O3) M-Monox-L X-Enzyme (xylanase) S-Sodium hydrosulfite (Na2S2O4) SO2-SO2 Add other notation for bleaching/brightening stages not represented above.	Enter numeric value	Enter numeric value for air dried tons of bleached pulp per day (ADTBP/d)	How does the mill use the bleached pulp produced? Determine the approximate decimal percentage requested based on annual bleached pulp capacity (ADTBP/yr). This column represents the amount of bleached pulp that is sold (or transferred to another mill within the same company) as bleached market pulp.	This column represents the amount of bleached pulp that is used onsite to manufacture bleached paper/paperboard.
Survey reference:										

Field:	NEI Site ID	Bleaching line ID (if applicable)	Are chlorine or chlorinated compounds used in any stage of the bleaching line?	Is the bleaching line preceded by O2 delignification?	Is the process ECF, PCF or TCF?	Bleaching sequence	Bleach line operating hr/yr	2009 nominal daily bleached production capacity, ADTBP/d	Approximate decimal percentage of bleaching line capacity sold as bleached market pulp	Approximate decimal percentage of bleaching line capacity used to manufacture paper or paperboard onsite	Check (=1)
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Example entry:	99999	B1	yes	yes	ECF - elemental chlorine free	DED(DOP)	8500	16	0.15	0.85	1
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Include one row for each bleach
 For example, a mill that produces
UK = Unknown. NA = Not Applicable
 Note: The terms "bleaching" are

Instruction:	Select from list	Select from list	Select yes/no	Each bleaching stage includes the tower vent, washer hood, seal tank vent, chemical and steam mixers, and vacuum pumps	Select from list	Select from list	Select yes/no	Each bleaching stage includes the tower vent, washer hood, seal tank vent, chemical and steam mixers, and vacuum pumps	Select from list	Select from list	Select yes/no
Survey reference:											
Field:	Stage 3 chloroform control option(s) used to demonstrate subpart 5 compliance	Stage 3 chlorinated HAP control option used to demonstrate subpart 5 compliance	Does stage 4 use chlorine or chlorinated compounds?	Stage 4 control method	Stage 4 chloroform control option(s) used to demonstrate subpart 5 compliance	Stage 4 chlorinated HAP control option used to demonstrate subpart 5 compliance	Does stage 5 use chlorine or chlorinated compounds?	Stage 5 control method	Stage 5 chloroform control option(s) used to demonstrate subpart 5 compliance	Stage 5 chlorinated HAP control option used to demonstrate subpart 5 compliance	Does stage 6 use chlorine or chlorinated compounds?
Example entry:	Meet effluent guidelines/standards	99% reduction (by weight) measured as total chlorinated HAP	Yes	SCBR_BL2	Meet effluent guidelines/standards	Outlet concentration < 10 ppmv measured as methanol					

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Expiration Date:
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Include one row for each bleach
 For example, a mill that produces
UK = Unknown. NA = Not Applicable
 Note: The terms "bleaching" are

<p>Each bleaching stage includes the tower vent, washer hood, seal tank vent, chemical and steam mixers, and vacuum pumps</p> <p>Instruction: Select from list</p> <p>Survey reference: Select from list</p>	<p>Select from list or write in description. Select "NA" if ClO2 bleaching is not performed at the mill. Select "None" if ClO2 bleaching is performed but no measures are employed to reduce CO emissions. Otherwise, describe process or control measure used to reduce CO emissions. Optional. Enter any comments you have on the data supplied.</p>
<p>Field:</p> <p>Stage 6 control method</p> <p>Stage 6 chloroform control option(s) used to demonstrate subpart S compliance</p> <p>Stage 6 chlorinated HAP control option used to demonstrate subpart S compliance</p>	<p>For mills that use chlorine dioxide (ClO2) bleaching, describe any process or control measures used to reduce emissions of carbon monoxide (CO) from bleaching processes.</p> <p>Comments</p>

Example entry:

None (no CO control measure)

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OMB Control No: xxxx-xxxx
 Expiration Date: xx/xx/xxxx

Did any of the responses (individual cells) you entered in this tab contain CBI?
 If yes, be sure to shade the CBI-containing cells red and follow the instructions in section C of the survey overview document for submitting CBI.

[Review Draft](#)

Provide data for the 2009 operating year. Do not include pulp dryers in this tab.

UK = Unknown. NA = Not Applicable. See instruction document for details on use of these terms.

Include one (or more) rows for each paper machine. You may include multiple rows for each paper machine if needed to reflect information that varies considerably by major paper grade, copying down information that does not vary (or remains adequately representative) from row to row.

Field:	NEI Site ID	Paper machine Emission Unit ID	Type of paper machine as currently configured	Is furnish mixture bleached or unbleached?	Hardwood kraft %	Softwood kraft %	Soda %	Sulfite %	Dissolving/specialty pulp %	Semichemical pulp %	Hardwood mechanical/groundwood %	Softwood mechanical/groundwood %	Secondary fiber %
Instruction: Survey reference:	Provide for all entries. This should match NEI Site ID used in Part II.			Complete table for operable paper machines located at any type of mill. You may need to specify the same paper machine in multiple rows if the machine produces multiple grades of paper at different times (see instructions).	Select paper machine configuration from the menu or write in Select from menu	Specify the approximate fiber makeup of each paper machine furnish. Indicate the makeup by showing an approximate percentage in decimal form (e.g., enter 0.65 for 65% softwood kraft). You may specify a range (e.g., 0.6-0.7) if there is variation within a main paper grade. Pulp types used							
Example entry:	99999	PM1	Fourdrinier	bleached	0.2	0.65							0.15
	99999	PM1	Fourdrinier	bleached	0.3-0.4	0.6-0.7							

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OMB Control No:
 Expiration Date:
 Review Draft

Provide data for the 200:
 UK = Unknown. NA = I
 Include one (or more) ro

<p>Indicate the other pulp type(s) followed by its approximate decimal percentage (e.g., softwood semichem - 0.10)</p> <p>Instruction: Survey reference:</p>	<p>Select from menu the most closely related paper grade(s) produced by the paper machine.</p> <p>If multiple paper grades are produced on the same machine, add the additional paper grade(s) in separate rows for the paper machine. Add rows for the major paper grades listed in the pull down menu only (not for every single minor variation within every major paper grade).</p> <p>Enter paper machine nominal production capacity in air dried tons paper/day (ADT/d)</p> <p>Specify high density pulp storage (stock chest) consistency in decimal form (e.g., enter 0.15 for 15%).</p> <p>Leave blank for bleached pulp.</p> <p>Select yes/no. If yes, please include an explanation.</p> <p>Leave blank for bleached pulp.</p> <p>Specify the headbox consistency in decimal form (e.g., enter 0.001 for 0.1%)</p>	<p>Enter the numeric value for the white water recirculation rate in gallons per oven dried ton of pulp (gal/ODTP). This is the amount of recirculated white water added to the pulp stock prior to the paper machine headbox/wet end.</p> <p>Provide typical white water methanol concentration in milligrams per liter (mg/l) if it has been measured.</p> <p>HAP concentrations at the paper machine wet end are of interest.</p> <p>Provide typical white water acetaldehyde concentration in milligrams per liter (mg/l) if it has been measured</p> <p>Specify HAPs and concentrations if known. You may provide documentation of typical white water HAP concentrations (if measured) as a separate attachment to your survey response.</p>
<p>Field: Non-wood fiber % Other % (specify)</p> <p>Example entry:</p>	<p>Paper grade produced</p> <p>coated free sheet uncoated free sheet</p> <p>Nominal production capacity, ADT/d</p> <p>935 1050</p> <p>For unbleached pulps, what is the consistency of pulp in high density storage (%)?</p> <p>0.001 0.001</p> <p>For unbleached pulps, has the mill taken steps (e.g., installed a screw press) to raise the consistency of the pulp in high density storage in order to reduce emissions associated with the fluid in the unbleached pulp?</p>	<p>White water recirculation rate, gal/ODTP</p> <p>48,300 48,300</p> <p>White water methanol concentration, mg/l (if known)</p> <p>28 28</p> <p>White water acetaldehyde concentration, mg/l (if known)</p> <p>UK UK</p> <p>White water other HAP concentration, mg/l (if known)</p> <p>UK UK</p>

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Provide data for the 200:
UK = Unknown. NA = I
 Include one (or more) ro

<p>Enter description. Examples may include: measures to reduce organics in the pulp stock liquid or white water (e.g., use of clean condensates in final stage of pulp washing); or switching to non-HAP or reduced-HAP additives.</p> <p>Note Emission Unit ID of stripper if used to strip organics from the paper machine white water (or pulping liquid). Strippers should be included in the Equip detail tab.</p>	<p>Enter the number of vents/stacks on the paper machine wet end (e.g., forming and press sections, and other portions of paper machine prior to first dryer) that vent to the atmosphere. Count vents ducted together prior to release to the atmosphere as one vent (e.g., count 4 vacuum system vents ducted together prior to release to the atmosphere as one vent stack).</p>	<p>Enter the total exhaust gas flow rate from the wet end vents/stacks in actual cubic feet per minute (if known)</p>	<p>Specify APCD_ID from the <i>PI Controls</i> tab, if applicable (e.g., if an APCD is used on wet end vent gases).</p>	<p>Enter number of dryer steam cylinders</p>	<p>Select air dryer firing method from menu or write in.</p> <p>Air dryers are direct fired or indirect-fired (use steam-to-air heat exchangers to produce a hot air stream that is forced over the surface of the paper). Hoods are used to contain and route the air flow. Air dryers tend to be used on lighter weights of paper, such as tissues, and to supplement the drying of steam cylinders.</p>	<p>Enter the number of vents/stacks on the paper machine associated with the paper machine dryer(s). Count vents ducted together prior to release to the atmosphere as one vent (e.g., count 4 dryer system vents ducted together prior to release to the atmosphere as one vent stack).</p>	<p>Enter the total exhaust gas flow rate from the dryer vents/stacks in actual cubic feet per minute (if known)</p>	<p>Specify APCD_ID from the <i>PI Controls</i> tab if applicable (e.g., if an APCD is used on dry end vent gases)</p>
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Field:	Describe any process improvements used to reduce HAP emissions from the wet end	Number of vents/stacks on the wet end	Total exhaust gas flow rate from the wet end vents/stacks, acfm (if known)	Add-on air pollution controls used to reduce HAP emissions from the wet end (insert APCD_IDs)	Number of dryer steam cylinders	Indicate firing method and fuel type if air drying is used	Number of dryer vents/stacks	Total exhaust gas flow rate from the dryer vents/stacks, acfm (if known)	Add-on air pollution controls used to reduce HAP emissions from the dryers (insert APCD_IDs)
Example entry:		16	456,000		50	steam-heated (indirect-fired)	4	90,000	
		16	456,000		50	steam-heated (indirect-fired)	4	90,000	

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OMB Control No:
Expiration Date:
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Provide data for the 200:
UK = Unknown. NA = I
 Include one (or more) ro

Enter the number of vents/stacks on the paper machine dry end following the dryers (e.g., vents around the calendering and winding areas) that vent to the atmosphere. Count vents ducted together prior to release to the atmosphere as one vent.

Enter the total exhaust gas flow rate from dry end vents/stacks not associated with the paper machine dryer(s) in actual cubic feet per minute (if known)

Enter description of any process improvements that might reduce HAP emissions from the paper machine dry end (dryers or other vents/stacks following the dryers).

Optional. Enter any comments you have on the data supplied.

Instruction:
Survey reference:

Field:	Number of vents/stacks following the dryer	Total exhaust gas flow rate from the dry end vents/stacks, acfm (if known)	Describe any process improvements used to reduce HAP emissions from the dry end	Comments
Example entry:	2	40,000		
	2	40,000		

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OMB Control No: XXXX-XXXX
 Expiration Date: XXXX-XXXX
 Review Draft

Did any of the responses (individual cells) you entered in this tab contain CBI?
 If yes, be sure to shade the CBI-containing cells red and follow the instructions in section C of the survey overview document for submitting CBI.

WWTP = wastewater treatment plant
 Provide a flow diagram of each WWTP showing each wastewater handling/treatment unit.
 UK = Unknown, NA = Not Applicable. See instruction document for details on use of these terms.
 Use this table to specify any Federal/State/local requirements, permit limits, fence-line monitoring, measurement methods, or modeling methods that apply for measurement or estimation of air emissions (HAP, TRS including H2S) associated with the WWTP.

<p>Instruction: Survey reference:</p>	<p>Provide for all entries. This should match NEI Site ID used in Part II.</p>	<p>Select yes or no. If yes, please continue with completion of the WW tab. If no, see the instruction document.</p>	<p>Select from menu or write in.</p>	<p>Select from menu: Yes - Biological treatment occurring at the wastewater treatment entity (POTW or private company) is used to comply with the subpart 5 standards for kraft condensates. OR No - The mill uses a methods other than biological treatment to comply with the kraft condensate standards. If you answer yes, then EPA requests that you complete the remainder of this WW tab to the extent that information is available for the WWTP.</p>	<p>Specify yes/no.</p>	<p>Select yes or no. If yes, submit the most recent measurement methods and results as a separate file attachment to your survey response.</p>	<p>Select yes or no. If yes, submit the most recent measurement methods (e.g., ambient measurements) and results as a separate file attachment to your survey response.</p>	<p>Select yes or no. If yes, submit documentation of the most recent modeled emission estimates as a separate file attachment to your survey response.</p>	<p>Select not applicable "NA" from menu if you answered yes to one of the previous 3 questions. Select from menu if air emissions associated with wastewater treatment are not addressed in your air permit. Enter the 2009 average daily throughput of the wastewater treatment plant (million gallons per day)</p>
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<p>Field:</p>	<p>NEI Site ID</p>	<p>Does the mill perform onsite wastewater treatment beyond operation of a clarifier for suspended solids removal?</p>	<p>If mill wastewater treatment is outsourced to a POTW or private entity, indicate pre-treatment steps occurring onsite at the mill.</p>	<p>For kraft pulp mills outsourcing wastewater treatment, is biological treatment performed at the WWTP used to demonstrate compliance with the subpart 5 kraft condensate standards?</p>	<p>Does the mill have permit limits (including occupational health limits) related to air pollutants specifically from wastewater sources?</p>	<p>If yes, please specify the limits (and applicable units) and explain how compliance is demonstrated with these limits.</p>	<p>Has fence-line monitoring for air emissions (including WWTP air emissions) been performed since the mill came into compliance with the cluster rules (NESHAP subpart 5 and the pulp and paper effluent limitations)?</p>	<p>Have air emissions associated with the WWTP been measured?</p>	<p>Have air emissions associated with the WWTP been estimated (e.g., with 40 CFR part 63 Appendix C and WATERS or another model)? Explain how wastewater treatment system emissions are accounted for in your air permit. If you answered "no" to the previous 3 questions</p>	<p>WWTP throughput, MGD/day</p>
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<p>Example entry:</p>	<p>99999</p>	<p>yes</p>		<p>yes</p>	<p>We have OSHA limits for H2S and other compounds. See WWTP attachment with our survey response for a tabular summary.</p>	<p>no</p>	<p>no</p>	<p>yes (see separate WWTP attachment with modeling input and output)</p>	<p>NA</p>	<p>18.5</p>
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OMB Control No:
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WWTP = wastewater treatment plant
 Provide a flow diagram of each WWTP
 UK = Unknown, NA = Not Applicable
 Use this table to specify any Federal/

If known, enter the approximate volume percentage of water entering the WWTP from each general mill location. Use decimal percentages (e.g., enter 0.75 for 75%).
 See the instruction document for joint WWTPs shared by multiple mills.

Instruction:
Survey reference:

Field:	Approximate volume percentage of WWTP capacity from kraft condensate streams hard piped for biological treatment in the WWTP (per subpart S) (if known)	Approximate volume percentage of WWTP capacity from chemical pulping and chemical recovery processes (other than subpart S hard-piped kraft condensates) (if known)	Approximate volume percentage of WWTP capacity from non-chemical pulping processes (e.g., mechanical, secondary fiber, or non-wood pulping) (if known)	Approximate volume percentage of WWTP capacity from the power and steam generation area(s) (e.g., boiler blowdown, wet ash handling systems) (if known)	Approximate volume percentage of WWTP capacity from bleaching processes (if known)	Approximate volume percentage of WWTP capacity from papermaking processes (if known)	Approximate volume percentage of WWTP capacity from other processes (if known)	Check (=1)	General type of wastewater treatment system	Identify upstream process wastewater treatment systems that reduce wastewater treatment unit air emissions of nonchlorinated organic HAP and TRS (including H2S).	Describe any upstream practices or pollution prevention measures that reduce wastewater treatment unit air emissions of nonchlorinated organic HAP and TRS (including H2S).	Describe any upstream practices or pollution prevention measures that reduce wastewater treatment unit air emissions of chlorinated HAP.	List the wastewater treatment units in your WWTP in the general sequence in which they are used
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Example entry:	0.05	0.25	NA	0.05	0.2	0.35	0.1	1	Aerated stabilization basin (aerated surface impoundment)	steam stripper (STRIPPER)	Use ClO2 bleaching (instead of chlorine or hypochlorite)	Clarifiers 1-3 (in parallel), aeration basins 1 and 2, activated sludge basin, and secondary clarifiers 4-6 (in parallel)
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OMB Control No: Expiration Date: Review Draft		Biological treatment system performance data (required for biological treatment systems controlling kraft pulping condensates):																																								
WWTP = wastewater treatment plant Provide a flow diagram of each WWTP UK = Unknown, NA = Not Applicable Use this table to specify any Federal/E		This question applies for non-thoroughly mixed biological treatment units. Specify the number of zones used to characterize the biological treatment system (e.g., under 40 CFR part 63, Appendix C). Enter "NA" if not applicable.																																								
Instruction: Survey reference:		Enter the percent reduction of total HAP if percent reduction is used to demonstrate compliance with subpart S. For example, enter "92" for a 92 percent reduction. Leave blank if the percent reduction compliance option is not used.					The value of $F_{in}(MeOH)$ is used in the equations in §63.457(l) of subpart S for purposes of determining percent reduction or mass removal of total HAP in a biological treatment system. "Total HAP" includes acetaldehyde, methanol, MEK, and propionaldehyde.					Enter the mass removal of total HAP if mass removal is used to demonstrate compliance with subpart S. Leave blank if the mass removal compliance option is not used.																														
Field:		<table border="1"> <thead> <tr> <th>Number of zones used to characterize the biological treatment system</th> <th>Q1 mass flow rate of methanol entering the system (kg/Mg ODP)</th> <th>Q1 mass flow rate of acetaldehyde, MEK, and propionaldehyde entering the system (kg/Mg ODP)</th> <th>Mass flow ratio of non-methanol total HAP to methanol (value of "r")</th> <th>Q1 value of $F_{in}(MeOH)$ determined according to 40 CFR 63 Appendix C</th> <th>Q1 percent reduction in "total HAP" (%)</th> <th>Q1 mass removal of "total HAP" (kg/Mg ODP)</th> <th>Q2 mass flow rate of methanol entering the system (kg/Mg ODP)</th> <th>Q2 value of $F_{in}(MeOH)$ determined according to 40 CFR 63 Appendix C</th> <th>Q2 percent reduction in total HAP (calculated using the quarterly methanol measurement and value of "r" as specified in subpart S), %</th> <th>Q2 mass removal of "total HAP" calculated as specified in subpart S (kg/Mg ODP)</th> <th>Q3 mass flow rate of methanol entering the system (kg/Mg ODP)</th> <th>Q3 value of $F_{in}(MeOH)$ determined according to 40 CFR 63 Appendix C</th> <th>Q3 percent reduction in total HAP (calculated using the quarterly methanol measurement and value of "r" as specified in subpart S), %</th> </tr> </thead> <tbody> <tr> <td>4</td> <td>11.5</td> <td>0.35</td> <td>0.03</td> <td>0.97</td> <td>94</td> <td></td> <td>5.9</td> <td>0.92</td> <td></td> <td>5.3</td> <td>9.8</td> <td>0.98</td> <td>95</td> </tr> </tbody> </table>													Number of zones used to characterize the biological treatment system	Q1 mass flow rate of methanol entering the system (kg/Mg ODP)	Q1 mass flow rate of acetaldehyde, MEK, and propionaldehyde entering the system (kg/Mg ODP)	Mass flow ratio of non-methanol total HAP to methanol (value of "r")	Q1 value of $F_{in}(MeOH)$ determined according to 40 CFR 63 Appendix C	Q1 percent reduction in "total HAP" (%)	Q1 mass removal of "total HAP" (kg/Mg ODP)	Q2 mass flow rate of methanol entering the system (kg/Mg ODP)	Q2 value of $F_{in}(MeOH)$ determined according to 40 CFR 63 Appendix C	Q2 percent reduction in total HAP (calculated using the quarterly methanol measurement and value of "r" as specified in subpart S), %	Q2 mass removal of "total HAP" calculated as specified in subpart S (kg/Mg ODP)	Q3 mass flow rate of methanol entering the system (kg/Mg ODP)	Q3 value of $F_{in}(MeOH)$ determined according to 40 CFR 63 Appendix C	Q3 percent reduction in total HAP (calculated using the quarterly methanol measurement and value of "r" as specified in subpart S), %	4	11.5	0.35	0.03	0.97	94		5.9	0.92		5.3	9.8	0.98	95
Number of zones used to characterize the biological treatment system	Q1 mass flow rate of methanol entering the system (kg/Mg ODP)	Q1 mass flow rate of acetaldehyde, MEK, and propionaldehyde entering the system (kg/Mg ODP)	Mass flow ratio of non-methanol total HAP to methanol (value of "r")	Q1 value of $F_{in}(MeOH)$ determined according to 40 CFR 63 Appendix C	Q1 percent reduction in "total HAP" (%)	Q1 mass removal of "total HAP" (kg/Mg ODP)	Q2 mass flow rate of methanol entering the system (kg/Mg ODP)	Q2 value of $F_{in}(MeOH)$ determined according to 40 CFR 63 Appendix C	Q2 percent reduction in total HAP (calculated using the quarterly methanol measurement and value of "r" as specified in subpart S), %	Q2 mass removal of "total HAP" calculated as specified in subpart S (kg/Mg ODP)	Q3 mass flow rate of methanol entering the system (kg/Mg ODP)	Q3 value of $F_{in}(MeOH)$ determined according to 40 CFR 63 Appendix C	Q3 percent reduction in total HAP (calculated using the quarterly methanol measurement and value of "r" as specified in subpart S), %																													
4	11.5	0.35	0.03	0.97	94		5.9	0.92		5.3	9.8	0.98	95																													
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OMB Control No:
Expiration Date:
[Review Draft](#)

WWTP = wastewater treatment plant
 Provide a flow diagram of each WWTP
 UK = Unknown, NA = Not Applicable
 Use this table to specify any Federal/

Instruction: Fourth quarter (Q4) compliance Optional. Enter any comments you have on the data supplied.

Survey Reference:

Field:	Q3 mass removal of "total HAP" calculated as specified in subpart 5. (kg/Mg ODP)	Q4 mass flow rate of methanol entering the system (kg/Mg ODP)	Q4 value of $F_{in}(MeOH)$ determined according to 40 CFR 63 Appendix C	Q4 percent reduction in total HAP (calculated using the quarterly methanol measurement and value of "r" as specified in subpart 5). %	Q4 mass removal of "total HAP" calculated as specified in subpart 5 (kg/Mg ODP)	Comments
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Example entry: 12.3 0.95 92

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OMB Control No: xxxx-xxxx
 Expiration Date: xx/xx/xxxx

[Review Draft](#)

Did any of the responses (individual cells) you entered in this tab contain CBI?
 If yes, be sure to shade the CBI-containing cells red and follow the instructions in section C of the survey overview document for submitting CBI.

If you are required to submit a Part III response, are you deferring until Part III submittal of any of the test data required in Attachment 1 to the Part I survey instructions?

Use this table to identify the specific emission units for which emission test reports are being submitted. EPA will extract the test data from the emission test reports.

UK = Unknown. NA = Not Applicable. See instruction document for details on use of these terms.

See Attachment 3 of the Part I survey instruction document for a list of emissions test reports to be submitted.

	Leave columns that do not apply for a given emission unit blank.					
Instruction:	Provide for all entries. This should match NEI Site ID used in Part II.	Provide for all entries. Emission Unit IDs should match those used in other tabs such as the <i>PI Equip detail</i> tab.	Specify the collection system if applicable. (Examples of collection systems include closed vent systems, LVHC, and HVLC systems.) Collection system IDs should match those used in other tabs such as the <i>PI Equip detail</i> tab.	Provide the APCD used during the emissions test. APCD IDs should match those used in other tabs such as the <i>PI Equip detail</i> tab (unless equipment configuration has changed).	Enter combustion controls used during the emission test (e.g., combustion modifications/controls specified in the <i>PI Equip detail</i> tab)	Enter year testing was conducted (i.e., the test date year)
Survey reference:	Use this column for notes or if helpful to specify the emission points tested (e.g., for equipment with multiple emission points, where only selected emission points/vents were tested)					

Field:	NEI Site ID	Emission Unit ID(s)	Collection system ID(s)	APCD ID(s)	Combustion modifications or controls used to reduce air pollution (from combustion sources)	Process testing notes (optional)	Test report year (XXXX)
Example entry:		99999 DIG-1, DIG-2, EVAP 99999 LK1	LVHC-1	LK1/SCBR2 SCBR2			2006 2006

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Field:	NEI Site ID	Emission Unit ID(s)	Collection system ID(s)	APCD_ID(s)	Combustion modifications or controls used to reduce air pollution (from combustion sources)	Process testing notes (optional)	Test report year (XXXX)
51							
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OMB Control No:

Expiration Date:

[Review Draft](#)

Use this table to identify the specific
UK = Unknown. NA = Not Applicable
See Attachment 3 of the Part I surve

Instruction:	List the pollutants tested. Separate multiple pollutants by commas.	Enter the EPA test method number (e.g., M5, M7E). Be very specific if the method used was not an EPA method.	Specify if APCD inlet or outlet data are provided (or both)	This question will be used in determining whether the test data remain representative of your current operations.	Explain any changes in equipment configuration as they relate to representativeness of the emissions test data supplied.	OPTIONAL: Data regarding frequency and cost of testing would help EPA more accurately estimate testing costs associated with the pulp and paper NESHA and NSPS.	OPTIONAL	Optional. Enter any comments you have on the data supplied.
Field:	Pollutants tested	Test method(s) used	Are inlet or outlet data provided?	Has the configuration of the emission unit, combustion controls, collection system, or APCD changed since the test was conducted?	If yes, please explain	How often are you required to perform testing of this emission unit for the pollutants listed?	Approximate cost per test, \$	Comments
Example entry:	methanol PM	M308 M5	inlet and outlet outlet	no no		one-time test only annually	12000 6000	

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Drop Down List	Field	NOTE
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Frequently Used Drop Downs

Yes No	CBI Box All tabs but Permit Limits	All tabs but Permi
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yes no UK	Small business	Mill
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Applies NA NA-Synthetic Area Source	P&P NESHAP subpart S Combustion Source NESHAP subpart MM Paper/web coating NESHAP subpart JJJ Other NESHAP (list subparts)	Mill Mill Mill
---	---	----------------------

Applies NA	Kraft NSPS subpart BB	Mill
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Yes No	Has the mill taken steps within the last 10 years to control makeup water quality for the causticizing emission unit such that air emissions from any equipment would be reduced?	equip
	Is the stripper integrated with the multiple effect evaporator system?	equip
	Is emission unit subject to NESHAP subpart S?	equip
	Is emission unit subject to NSPS BB?	Mill
	Does the mill purchase secondary fiber pulp?	Mill
	Is natural gas supply currently available to the mill (e.g., truck delivery or pipeline)?	Mill
	Does the mill purchase virgin pulp?	Mill
	Does the mill produce virgin pulp?	controls
	Heat recovery	controls
	Is WESP preceded by a quench chamber	controls
	Have fields/chambers been added to expand the ESP within the last 10 years?	controls
	Is water recirculated?	pulp
	Sawmill residues	pulp
	Chips produced offsite	pulp
	Chips produced onsite	pulp
	For TMP or pressurized groundwood systems, is a heat recovery system used?	bleaching
	Is the bleaching line preceded by O2 delignification?	bleaching
	Are chlorine or chlorinated compounds used in any stage of the bleaching line?	bleaching
	Does stage 6 use chlorine or chlorinated compounds?	bleaching
	Does stage 5 use chlorine or chlorinated compounds?	bleaching
	Does stage 4 use chlorine or chlorinated compounds?	bleaching
	Does stage 3 use chlorine or chlorinated compounds?	bleaching
	Does stage 2 use chlorine or chlorinated compounds?	bleaching
	Does stage 1 use chlorine or chlorinated compounds?	WW
	Have air emissions associated with the WWTP been estimated (e.g., with 40 CFR part 63 Appendix C and WATER9 or another model)?	WW
	Have air emissions associated with the WWTP been measured?	WW
	Has fenceline monitoring for air emissions (including WWTP air emissions) been performed since the mill came into compliance with the cluster rules (NESHAP subpart S and the pulp and paper effluent limitations)?	WW
	Does the mill have permit limits (including occupational health limits) related to air pollutants specifically from wastewater sources?	Emission
	Has the configuration of the emission unit, combustion controls, collection system, or APCD changed since the test was conducted?	Emission
	If you are required to submit a Part III response, are you deferring until Part III	

Mill Tab

HAP size classification

major
area (true)
synthetic minor
UK

Primary NAICS

322110-Pulp Mills
322121-Paper (except Newsprint) Mills
322122-Newsprint Mills
322130-Paperboard Mills
322211-Corrugated and Solid Fiber Box Manufacturing
322212-Folding Paperboard Box Manufacturing
322213-Setup Paperboard Box Manufacturing
322214-Fiber Can, Tube, Drum, and Similar Products Manufacturing
322215-Non-Folding Sanitary Food Container Manufacturing
322221-Coated and Laminated Packaging Paper Manufacturing
322222-Coated and Laminated Paper Manufacturing
322223-Coated Paper Bag and Pouch Manufacturing
322224-Uncoated Paper and Multiwall Bag Manufacturing
322225-Laminated Aluminum Foil Manufacturing for Flexible Packaging Uses
322226-Surface-Coated Paperboard Manufacturing
322231-Die-Cut Paper and Paperboard Office Supplies Manufacturing
322232-Envelope Manufacturing
322233-Stationery, Tablet, and Related Product Manufacturing
322291-Sanitary Paper Product Manufacturing
322299-All Other Converted Paper Product Manufacturing

Worldwide employees
Facility employees

<50
50-99
100-499
500-749
750-999
>1000

Boiler NESHAP subpart DDDDD (or CISWI emission guidelines/NSPS) that are under development

Expect DDDDD to apply
Expect CISWI to apply

Expect DDDDD and/or CISWI to apply (to be determined based on final applicability of these rules)
NA

Boiler NSPS

D
Da
Db
Dc

Other NSPS (list subparts)

K
Ka
Kb
GG
Other (enter 40 CFR part 60 subpart)
NA

Does the mill produce pulp from secondary fiber?

yes
yes - use pre-consumer fiber
yes - use post-consumer fiber
yes - use pre- and post-consumer fiber
no

Types of market pulp produced by the mill

Dissolving pulp
Softwood chemical market pulp
Hardwood chemical market pulp

Mechanical market pulp
Market pulp from secondary (recycled) fiber
NA (market pulp not produced)

Is bleaching or brightening performed at the mill?

yes-bleaching
yes-brightening
yes-bleaching and brightening
yes-other {specify}
no

newsprint	Paper grade 1
coated free sheet	Paper grade 2
uncoated free sheet	Paper grade 3
coated groundwood	Paper grade 4
uncoated groundwood	Paper grade 5
tissue & sanitary	Paper grade 6
specialty packaging & industrial	Paper grade 7
kraft packaging	Paper grade 8
linerboard	Paper grade 9
corrugating medium	Paper grade 10
solid bleached board	
recycled board	
construction paper and board	
other {specify type}	

PI Equip detail Tab

Configuration if not emitted through a conveyance

NV
BLDG
FUGITIVE

Year emission unit installed

UK
pre-1990

Location of flow rate provided

inlet to collection system
collection system outlet prior to control device,
inlet to control device,
control device outlet
prior to atmospheric release

Combustion controls

low NOx burners
quaternary air
other {specify}

Recovery furnace ESP (dry bottom)	APCD1 type
Recovery furnace ESP (wet bottom)	APCD2 type
ESP (dry)	APCD3 type
Wet ESP (WESP)	APCD4 type
Scrubber - venturi	
Scrubber - quench	
Scrubber - packed bed	
Scrubber	
Absorber	
Mist eliminator	
Thermal oxidizer/incinerator	
Regenerative thermal oxidizer	
Multicyclone	
Cyclone (excluding product recovery cyclones)	
Fabric filter (baghouse)	
Condenser	
Gravel bed	

Dry sorbent injection
Carbon absorber
Selective noncatalytic reduction
Selective catalytic reduction
Boiler (specify Emission Unit ID)
Lime kiln (specify Emission Unit ID)
Recovery furnace (specify Emission Unit ID)
Other - specify type (and Emission Unit ID if applicable)
Uncontrolled

Reason subject to BB

new
modified
reconstructed
modified or reconstructed (not sure)
collects emissions from BB emission units

Specify TRS compliance option used to demonstrate NSPS subpart BB compliance (if applicable)
Specify TRS compliance option used for backup method of control (if applicable)

5 ppm_{dv} @ 10% O₂ (combustion control)
5 ppm_{dv}, uncorrected for O₂ (control other than combustion)
combust gases in lime kiln or recovery furnace subject to subpart BB
combust gases at 1200°F for at least 0.5 sec
incinerating brown stock washer gases is not feasible
uncontrolled digester gases contain <0.01 lb TRS/ton ADP
8 ppm_{dv} @ 10% O₂ (lime kilns)
0.033 lb/ton BLS as H₂S (SDTs)
5 ppm_{dv} @ 8% O₂ (straight recovery furnace)
25 ppm_{dv} @ 8% O₂ (cross recovery furnace)
Meet permit limit more stringent than NSPS

Subpart S compliance option used (for primary method of control)
Subpart S compliance option used (for backup method of control, if applicable)

Reduce total HAP emissions by 98 wt%

Reduce total HAP concentration at the outlet of thermal oxidizer to <20 ppm_v @ 10% O₂ (dry basis)

Reduce total HAP emissions using a thermal oxidizer operating >1600°F and >.75 secs residence time

Use a boiler, LK, or RF in which the HAP gas stream is introduced with the primary fuel into the flame zone

Use a boiler or RF with a heat input capacity >150 MMBtu/hr (44 MW) in which the HAP gas stream is introduced with the combustion air

Clean condensate alternative (§63.447).
0.89 lb/ton ODP (for Ca- or Na-based sulfite pulping)
92% reduction by weight (for Ca- or Na-based sulfite pulping)
2.2 lb/ton ODP (for Mg-based or NH₃-based sulfite pulping)
87% reduction by weight (for Mg-based or NH₃-based sulfite pulping)

Provide reason if not controlled to meet subpart S

Systems of this type at existing sources are not subject to subpart S
Mill is a synthetic area source
The system does not match the definitions for controlled systems in subpart S. Provide reason (e.g., due to specific location of the system in the process line).
Exception 63.443(a)(ii)(A): knotter system with HAP emissions <0.1 lb/ton ODP
Exception 63.443(a)(ii)(B): screen system with <0.2 lb/ton ODP.
Exception 63.443(a)(ii)(C): knotter and screen system with combined emissions <0.3 lb/ton ODP

Exception 63.443(a)(iv)(A): decker uses only fresh water or paper machine white water

Exception 63.443(a)(iv)(B): decker uses process water with < 400 ppm_w
Mill received equivalency by permit approval
Mill undertook innovations project
Emissions from this unit were offset using CCA
Other - specify

Batch or continuous

Batch
Continuous

HW SW HW/SW swing HW and SW Non-wood	Wood type (HW, SW, HW/SW swing)
--	---------------------------------

vacuum drum diffusion pressure belt	Washer types and sequence
--	---------------------------

contaminated condensates clean condensates white water other (specify) NA	Type of shower water used in decker
---	-------------------------------------

steam air	Type of stripper
--------------	------------------

TRS control BOD reduction water conservation subpart S kraft pulping condensate standards nonchlorinated organic HAP control	Primary reason for installation of the stripper
--	---

weak black liquor strong black liquor high density pulp white liquor green liquor	Tank contents
---	---------------

Open tank FR = fixed roof EFR = external floating roof IFR = internal floating roof Collection system and control device Emissions routed to process (enter Emission Unit ID)	Tank control technique
--	------------------------

NA Mechanical shoe primary seal (MS1) MS1 with shoe mounted secondary (MESA) MS1 with rim mounted secondary (MESA) liquid mounted primary seal (LM1) LM1 with rim mounted secondary (LM2) vapor mounted primary seal (VM1) M1 with rim mounted secondary (VM2)	If floating roof is used, type of seal
---	--

weak black liquor strong black liquor white liquor green liquor	Pond contents
--	---------------

<p>Untreated process condensates from {specify process - e.g., evaporator, blow heat recovery} surface water fresh water process water {specify source} treated wastewater partially treated wastewater {specify last wastewater treatment unit water passed through} mixture {specify sources}</p>	<p>Source(s) of makeup water added to mud washer or precoat filter</p>
---	--

<p>natural gas #2 distillate oil #6 residual oil bark hog fuel turpentine tall oil petroleum coke tire-derived fuel wastewater treatment plant residuals OCC rejects</p>	<p>Primary fuel type Supplemental fuel type 1</p>
--	--

<p>Btu/gal MMBtu/ton Btu/MMscf</p>	<p>Optional: Primary fuel HHV units Optional: Supplemental fuel type 1 HHV units</p>
--	---

<p>routine use (multi-fuel fired unit) startup backup shutdown pilot light during upset conditions seasonally during curtailments or peak prices when turpentine prices are low when tall oil prices are low</p>	<p>Conditions when supplemental fuel type 1 used</p>
--	--

<p>emission unit and control device operates in compliance with NSPS and NESHAP parameter limits during emission unit startup emission unit and control device operates during emission unit startup (but not necessarily in compliance with all NSPS/NESHAP parameter limits) backup/alternate control NA - applicable emission and parameter limits not expected to be exceeded during startup</p>	<p>Measures employed to reduce air emissions during emission unit startup (if any)</p>
---	--

<p>continue routing emissions to LVHC-1 collection system and primary or backup control system continue routing emissions to LVHC-1 collection system and primary or backup control system stop routing process condensates to stripper before beginning shutdown NA - applicable emission and parameter limits not expected to be exceeded during shutdown emission unit and control device operates during emission unit startup (but not necessarily in compliance with all NSPS/NESHAP parameter limits) continue routing emissions to LVHC-1 collection system and primary or backup control system Temperature drops below 200F</p>	<p>Measures employed to reduce air emissions during shutdown (if any)</p>
---	---

PI Permit limits

<p>TRS</p>	<p>Pollutant</p>
------------	------------------

SO2
sulfuric acid mist
NOx
CO
Pb or other HAP metals
VOC
THC
HCl
Methanol and gaseous organic HAP
Chlorine and chlorinated HAP
Opacity
PM
PM - filterable
PM - condensable
PM10
PM10 - filterable
PM10 - condensable
PM2.5
PM2.5 - filterable
PM2.5 - condensable

If the permit limit is identical to the Federal NESHAP or NSPS limit, you may enter the NESHAP/NSPS subpart here rather than restating the Federal limit in the columns to the right

Subpart S (P&P NESHAP)
Subpart MM (P&P combustion source NESHAP)
Subpart BB (Kraft NSPS)
Subpart BB (Kraft NSPS) - 1978
Subpart BB (Kraft NSPS) - 1986 revision

Units for permit limit 1 (including any applicable %O2 or %CO2 correction factors)

gr/dscf @ 8% O2
gr/dscf @ 10% O2
lb/ton BLS
ppmdv @ 8% O2
ppmdv @ 10% O2
lb/ton BLS (as H2S)
lb/MMBtu
ppmdv
% reduction
% opacity

3-hour	Averaging time for permit limit 1 (if applicable)
12-hour	Averaging time for permit limit 2 (if applicable)
daily	Averaging time for permit limit 3 (if applicable)
test	Averaging time for permit limit 4 (if applicable)
	Averaging time for permit limit 5 (if applicable)

PI Controls

Type of control device

Recovery furnace ESP (dry bottom)
Recovery furnace ESP (wet bottom)
ESP (dry)
Wet ESP (WESP)
Scrubber - venturi
Scrubber - quench
Scrubber - packed bed
Scrubber
Absorber
Mist eliminator
Thermal oxidizer/incinerator
Regenerative thermal oxidizer
Multicyclone
Cyclone (excluding product recovery cyclones)
Fabric filter (baghouse)
Condenser
Gravel bed

Dry sorbent injection
Carbon absorber
Selective noncatalytic reduction
Selective catalytic reduction
Other - *specify type*

Single-stage combustion chamber
Two-stage combustion chamber
Regenerative thermal oxidizer (RTO)

Incinerator type

preheat incoming emission stream
produce steam
produce hot water

What is the recovered heat from the incinerator exhaust used for?

activated carbon
lime
other (specify)

Sorbent type

acid gases (HCl, SO₂, HF)
SO₂
Hg
dioxins

List pollutants the sorbent injection was installed to control

Shake
Reverse air
Pulse jet

Bag cleaning method

surface water
fresh water
process water {specify source}
treated wastewater

partially treated wastewater {specify last wastewater treatment unit water passed through}
mixture {specify sources}

Water source

Treated in onsite wastewater treatment plant
Recycled to mud washer(s)
Recycled to SDT

Recycled to process: {specify equipment receiving water using Emission Unit ID OR APCD_ID}
POTW
Other {specify}

Wastewater (blowdown) reuse or disposal method

PM
PM and sorbent
Sorbent

Type of material collected

landfill onsite
landfill offsite
recycle to causticizing system
sent to salt cake mix tank
reuse {specify}

End use/method of disposal for solid material collected

<p>pressure drop liquid flow rate voltage current temperature (specify if inlet, outlet, bed, or other temperature) pH percent solids in recycle water other (specify)</p>	List continuous parameter monitoring systems used for this control device (e.g., pressure drop, liquid flow)
--	--

<p>Control device is started up and meets required operating parameter limits before emission unit is started up. Control device cannot be started prior to emission unit starting up due to safety issue or risk of property damage. {Explain} Control device cannot function as designed unless an air flow rate of {specify} acfm from the emission unit is achieved.</p>	<p>Explain how control device startup is integrated with (dependent upon) emission unit startup/operation</p>
--	---

<p>The applicable emission and parameter limits are expected to be met during startup</p>	<p>List any control device continuous emissions monitoring or operating parameter limits that cannot be met during control device startup</p>
---	---

<p>Control device continues to operate and meets required operating limits while emission unit is shut down. Control device cannot operate during emission unit shut down due to safety issue or risk of property damage. {Explain} Control device cannot function as designed unless an air flow rate of {specify} acfm from the emission unit is achieved.</p>	<p>Explain how control device shutdown is integrated with (dependent upon) emission unit shutdown</p>
--	---

Pulp prod

<p>kraft soda semi-chemical sulfite-NH3 sulfite-Ca Chemi-themo-mechanical pulp (CTMP) stone groundwood (SGW) pressurized groundwood (PGW) thermo-mechanical pulping (TMP) refiner mechanical pulping (RMP) secondary fiber non-wood</p>	<p>Pulping processes</p>
---	--------------------------

<p>cotton bagasse kenaf other {specify}</p>	<p>Non-wood material</p>
---	--------------------------

Byproducts

<p>batch continuous</p>	<p>Is tall oil acidulation reactor batch or continuous?</p>
-----------------------------	---

Kraft condensates

Digester systems Turpentine recovery systems Evaporator systems HVLC collection systems LVHC collection systems Combined systems Other systems {describe}	Kraft condensate stream
---	-------------------------

Yes No Partially	Is condensate stream collected and treated according to subpart S?
------------------------	--

NA-system does not exist at mill 1 2A 2B	Indicate volume reduction option being used, or other reason why condensate stream is not collected and controlled
---	--

92% total HAP reduction (by weight) Remove 6.6 pounds/ton ODP 210 ppmw at the outlet of the control device Remove 10.2 pounds/ton ODP 330 ppmw at the outlet of the control device Remove prorated mass of ___ pounds/ton ODP {specify limit}	For condensates treated by steam stripping, specify the control option used For condensates treated by biological treatment, specify the control option used Specify condensate treatment method (if other than steam stripping or biological treatment)
--	--

In series: As backup: Other:	Please describe if multiple treatment methods used for this condensate
------------------------------------	--

CCA

debit (uncontrolled) debit (under controlled) credit	CCA debit or credit generating emission point?
--	--

NA-debit source stand-alone biological treatment unit steam stripper other - specify	Clean condensate alternative technology applied
---	---

Bleaching

ECF - elemental chlorine free PCF - processed chlorine free TCF - totally chlorine free	Is the process ECF, PCF or TCF?
---	---------------------------------

HW only SW only	Material type
--------------------	---------------

mixture of HW and SW
secondary fiber
non-wood fiber

NA
scrubber {enter APCD_ID}
other {describe}

Stage 1 control method
Stage 2 control method
Stage 3 control method
Stage 4 control method
Stage 5 control method
Stage 6 control method

NA (no chlorine or chlorinated compounds used in this stage)
NA (mechanical, non-wood, or secondary fiber mill)
NA (synthetic area source)
Use no chlorine or hypochlorite AND meet effluent guidelines/standards
Use no chlorine or hypochlorite
Meet effluent guidelines/standards

Stage 1 chloroform control option(s) used to demonstrate subpart S compliance
Stage 2 chloroform control option(s) used to demonstrate subpart S compliance
Stage 3 chloroform control option(s) used to demonstrate subpart S compliance
Stage 4 chloroform control option(s) used to demonstrate subpart S compliance
Stage 5 chloroform control option(s) used to demonstrate subpart S compliance
Stage 6 chloroform control option(s) used to demonstrate subpart S compliance

NA (no chlorine or chlorinated compounds used in this stage)
NA (synthetic area source)
99% reduction (by weight) measured as total chlorinated HAP
99% reduction (by weight) measured as methanol
Outlet concentration < 10 ppmv measured as total chlorinated HAP
Outlet concentration < 10 ppmv measured as methanol
Total outlet mass emission levels for all subject stages < 0.002 lb/ton ODP

Stage 1 chlorinated HAP control option used to demonstrate subpart S compliance
Stage 2 chlorinated HAP control option used to demonstrate subpart S compliance
Stage 3 chlorinated HAP control option used to demonstrate subpart S compliance
Stage 4 chlorinated HAP control option used to demonstrate subpart S compliance
Stage 5 chlorinated HAP control option used to demonstrate subpart S compliance
Stage 6 chlorinated HAP control option used to demonstrate subpart S compliance

NA - ClO2 bleaching is not performed
None (no CO control measure)

For mills that use chlorine dioxide (ClO2) bleaching, describe any process or control measures used to reduce emissions of carbon monoxide (CO) from bleaching processes.

Paper prod

Fourdrinier
cylinder
twin-wire
other {specify}

Type of paper machine as currently configured

bleached
unbleached
mixture of bleached and unbleached (please specify)

Is furnish mixture bleached or unbleached?

coated free sheet
uncoated free sheet
coated groundwood
uncoated groundwood
tissue & sanitary

Paper grade produced

specialty packaging & industrial
kraft packaging
linerboard
corrugating medium
solid bleached board
recycled board
construction paper and board
other (specify type)

For unbleached pulps, has the mill taken steps (e.g., installed a screw press) to raise the consistency of the pulp in high density storage in order to reduce emissions associated with the fluid in the unbleached pulp?

no
yes {please explain}

Indicate firing method and fuel type if air drying is used

steam-heated (indirect-fired)
direct fired (natural gas)
direct-fired {specify fuel}

HAP additives

Units for amount

gal/day
lb/day
lb/ton paper
gal/year
lb/year

WW

Does the mill perform onsite wastewater treatment beyond operation of a clarifier for suspended solids removal?

Yes
No - Mill wastewater treatment is outsourced to a POTW
No - Mill wastewater treatment is outsourced to a separate wastewater treatment plant owned/operated by {enter company name}.
No - Other {please explain}

If mill wastewater treatment is outsourced to a POTW or private entity, indicate pre-treatment steps occurring onsite at the mill.

Primary clarification
Secondary clarification
Primary and secondary clarification
Other: {specify}

For kraft pulp mills outsourcing wastewater treatment, is biological treatment performed at the WWTP used to demonstrate compliance with the subpart S kraft condensate standards?

Yes - Biological treatment occurring at the wastewater treatment entity (POTW or private company) is used to comply with the subpart S standards for kraft condensates.
No - The mill uses a methods other than biological treatment to comply with the kraft condensate standards.

Explain how wastewater treatment system emissions are accounted for in your air permit if you answered "no" to the previous 3 questions

Air emissions associated with wastewater treatment are not addressed in the air operating permit.
NA

Aerated stabilization basin (aerated surface impoundment) Activated-sludge biological treatment Anaerobic treatment Packaged system (specify e.g., UNOX system) Other (specify)	General type of wastewater treatment system
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steam stripper (enter Emission Unit ID) biological treatment unit wastewater thermal oxidizer (enter Emission Unit ID) Other (specify)	Identify upstream process wastewater treatment systems that reduce wastewater treatment unit air emissions of nonchlorinated organic HAP and TRS (including H2S).
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Use only nonchlorinated bleaching compounds Use ClO2 bleaching (instead of chlorine or hypochlorite) Other (specify)	Describe any upstream practices or pollution prevention measures that reduce wastewater treatment unit air emissions of chlorinated HAP.
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PI Emissions test data

PM PM2.5-filterable PM2.5-cond. NOx SO2 CO methanol THC chlorine CDD/CDF POM/PAH Speciated HAP metals HCl TRS	Pollutants tested
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outlet inlet inlet and outlet	Are inlet or outlet data provided?
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annually every 2 years every 5 years one-time test only as requested by the permitting authority	How often are you required to perform testing of this emission unit for the pollutants listed?
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