

(b) The plan does not need to list the facility or corporate organizational structure that the owner or operator will use to manage the response, as required by §154.1035(b)(3)(iii).

(c) The owner or operator must ensure and identify, by contract or a method described in §154.1228, that the response resources required under §154.1035(b)(3)(iv) are available for a worst case discharge.

[USCG-1999-5149, 65 FR 40827, June 30, 2000]

**Subpart I—Response Plans for Other Non-Petroleum Oil Facilities**

SOURCE: CGD 91-036, 61 FR 7932, Feb. 29, 1996, unless otherwise noted.

**§ 154.1310 Purpose and applicability.**

This subpart establishes oil spill response planning requirements for an owner or operator of a facility that handles, stores, or transports other non-petroleum oils. The requirements of this subpart are intended for use in developing response plans and identifying response resources during the planning process. They are not performance standards.

**§ 154.1320 Response plan submission requirements.**

An owner or operator of a facility that handles, stores, or transports other non-petroleum oils shall submit a response plan in accordance with the requirements of this subpart, and with all sections of subpart F of this part, except §§154.1045 and 154.1047, which apply to petroleum oils.

**§ 154.1325 Response plan development and evaluation criteria for facilities that handle, store, or transport other non-petroleum oils.**

(a) An owner or operator of a facility that handles, stores, or transports other non-petroleum oils must provide information in his or her plan that identifies—

- (1) Procedures and strategies for responding to a worst case discharge of other non-petroleum oils to the maximum extent practicable; and
- (2) Sources of the equipment and supplies necessary to locate, recover, and mitigate such a discharge.

(b) An owner or operator of a facility that handles, stores, or transports other non-petroleum oils must ensure that any equipment identified in a response plan is capable of operating in the conditions expected in the geographic area(s) in which the facility operates using the criteria in Table 1 of appendix C of this part. When evaluating the operability of equipment, the facility owner or operator must consider limitations that are identified in the ACPs for the COTP zone in which the facility is located, including—

- (1) Ice conditions;
- (2) Debris;
- (3) Temperature ranges; and
- (4) Weather-related visibility.

(c) The owner or operator of a facility that handles, stores, or transports other non-petroleum oils must identify the response resources that are available by contract or other approved means as described in §154.1028(a). The equipment identified in a response plan must include—

- (1) Containment boom, sorbent boom, or other methods for containing oil floating on the surface or to protect shorelines from impact;
- (2) Oil recovery devices appropriate for the type of other non-petroleum oils handled; and
- (3) Other appropriate equipment necessary to respond to a discharge involving the type of oil handled.

(d) Response resources identified in a response plan under paragraph (c) of this section must be capable of commencing an effective on-scene response within the times specified in this paragraph for the applicable operating area:

	Tier 1 (hrs.)	Tier 2	Tier 3
Higher volume port area .....	6	N/A	N/A
Great Lakes .....	12	N/A	N/A
All other river and canal, inland, near-shore, and offshore areas .....	12	N/A	N/A

(e) A response plan for a facility that handles, stores, or transports other non-petroleum oils must identify response resources with firefighting capability. The owner or operator of a facility that does not have adequate firefighting resources located at the facility or that cannot rely on sufficient local firefighting resources must identify and ensure, by contract or other

approved means as described in §154.1028(a), the availability of adequate firefighting resources. The response plan must also identify an individual located at the facility to work with the fire department on other non-petroleum oil fires. This individual shall also verify that sufficient well-trained firefighting resources are available within a reasonable response time to a worst case scenario. The individual may be the qualified individual as defined in §154.1020 and identified in the response plan or another appropriate individual located at the facility.

(f) The response plan for a facility that is located in any environment with year-round preapproval for use of dispersants and that handles, stores, or transports other non-petroleum oils may request a credit for up to 25 percent of the worst case planning volume set forth by subpart F of this part. To receive this credit, the facility owner or operator must identify in the plan and ensure, by contract or other approved means as described in §154.1028(a), the availability of specified resources to apply the dispersants and to monitor their effectiveness. The extent of the credit will be based on the volumes of the dispersant available to sustain operations at the manufacturers' recommended dosage rates. Identification of these resources does not imply that they will be authorized for use. Actual authorization for use during a spill response will be governed by the provisions of the NCP and the applicable ACP.

#### APPENDIX A TO PART 154—GUIDELINES FOR DETONATION FLAME ARRESTERS

This appendix contains the draft ASTM standard for detonation flame arresters. Devices meeting this standard will be accepted by the Commandant (CG-522).

##### 1. Scope

1.1 This standard provides the minimum requirements for design, construction, performance and testing of detonation flame arresters.

##### 2. Intent

2.1 This standard is intended for detonation flame arresters protecting systems containing vapors of flammable or combustible liquids where vapor temperatures do not exceed 60 °C. For all tests, the test media defined in 14.1.1 can be used except where detonation flame arresters protect systems han-

dling vapors with a maximum experimental safe gap (MESG) below 0.9 millimeters. Detonation flame arresters protecting such systems must be tested with appropriate media (the same vapor or a media having a MESG no greater than the vapor). Various gases and their respective MESG are listed in attachment 1.

2.2 The tests in this standard are intended to qualify detonation flame arresters for all in-line applications independent of piping configuration provided the operating pressure is equal to or less than the maximum operating pressure limit specified in the manufacturer's certification and the diameter of the piping system in which the detonation arrester is to be installed is equal to or less than the piping diameter used in the testing.

NOTE: Detonation flame arresters meeting this standard as Type I devices, which are certified to be effective below 0 °C and which can sustain three stable detonations without being damaged or permanently deformed, also comply with the minimum requirements of the International Maritime Organization, Maritime Safety Committee Circular No. 373 (MSC/Circ. 373/Rev.1).

##### 3. Applicable Documents

###### 3.1 ASTM Standards<sup>1</sup>

A395 Ferritic Ductile Iron Pressure-Retaining Castings For Use At Elevated Temperatures.

F722 Welded Joints for Shipboard Piping Systems

F1155 Standard Practice for Selection and Application of Piping System Materials

###### 3.2 ANSI Standards<sup>2</sup>

B16.5 Pipe Flanges and Flanged Fittings.

###### 3.3 Other Documents

3.3.1 ASME Boiler and Pressure Vessel Code<sup>2</sup>

Section VIII, Division 1, Pressure Vessels  
Section IX, Welding and Brazing Qualifications.

3.3.2 International Maritime Organization, Maritime Safety Committee<sup>3</sup>

MSC/Circ. 373/Rev. 1—Revised Standards for the Design, Testing and Locating of Devices to Prevent the Passage of Flame into Cargo Tanks in Tankers.

3.3.3 International Electrotechnical Commission<sup>4</sup>

Publication 79-1—Electrical Apparatus for Explosive Gas Atmospheres.

##### 4. Terminology

4.1  $\Delta P/P_0$ —The dimensionless ratio, for any deflagration and detonation test of 14.3, of the maximum pressure increase (the maximum pressure minus the initial pressure), as measured in the piping system on the side

<sup>1</sup>Footnotes appear at the end of this article.